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Hydrogen Behavior and Mitigation Measures: State of Knowledge and Database from Nuclear Community

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AFP/GETTY - H₂ explosion at Fukushima
March 11, 2011

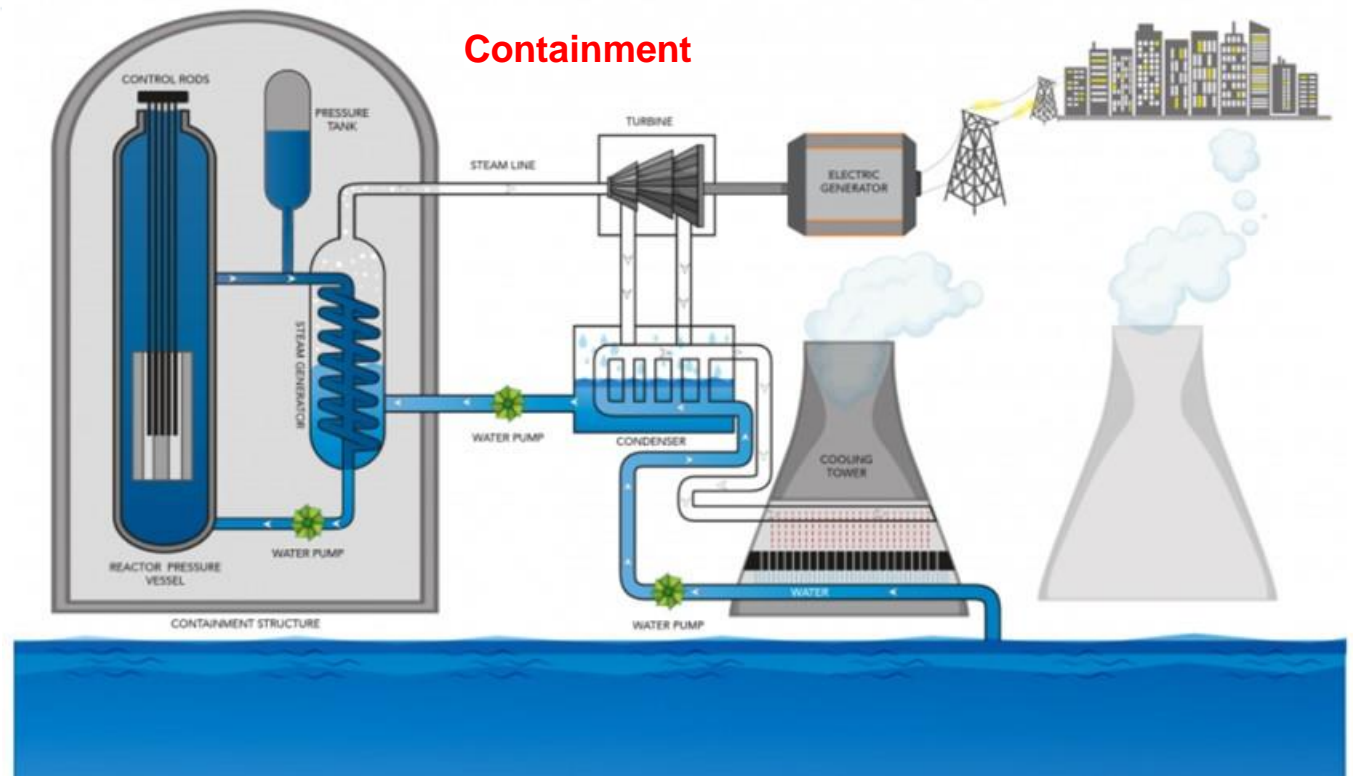


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Outline

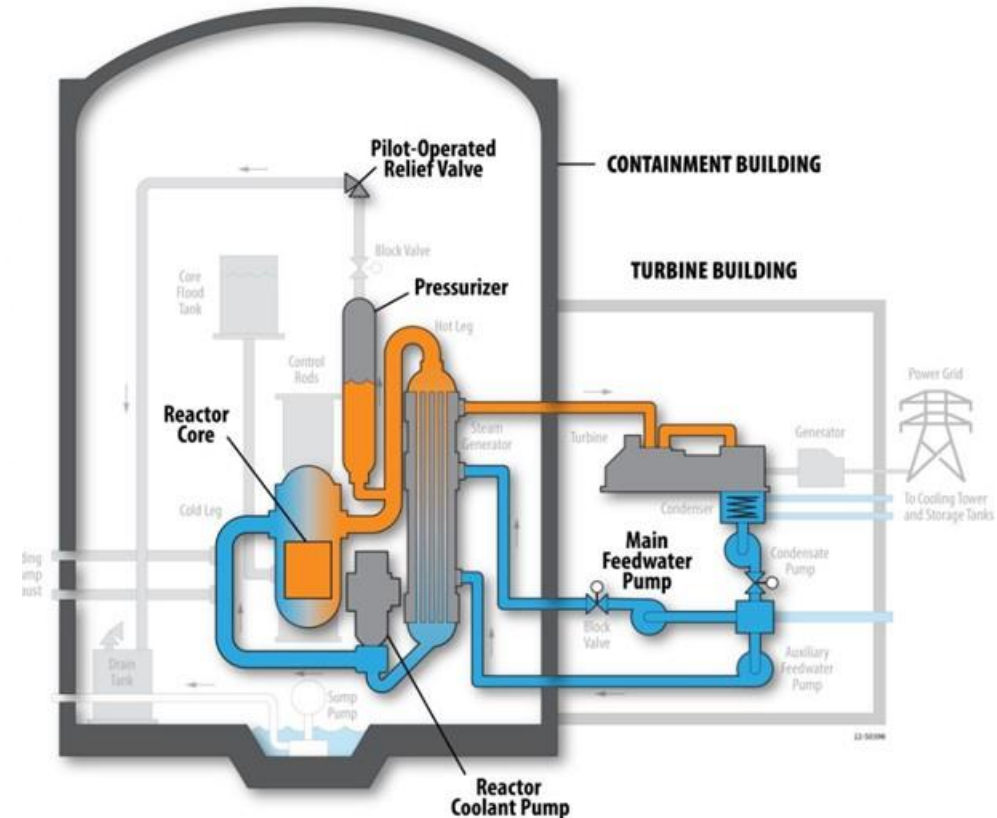
- Nuclear hydrogen safety
- R&D focus and evolution
- State of knowledge & Large-scale facilities
- Open issues and linkage to other industries



Schematic of Pressurized Water Reactor
[Graphic by Sarah Harman – U.S. Department of Energy](#)

Hydrogen Safety for Nuclear Reactors

- **Hydrogen can be produced from various sources in loss of coolant accidents**
 - Metal-steam reaction, molten core concrete interaction, water radiolysis
- **1979 Three Mile Island accident**
 - Estimated 4,500 m³ H₂ were generated by metal-steam reaction → H₂ deflagration occurred inside the containment → no damage to containment
- **2011 Fukushima Daiichi accident**
 - Estimated 5-10,000 m³ H₂ per reactor were generated → H₂ deflagration/detonation damaged three reactor buildings

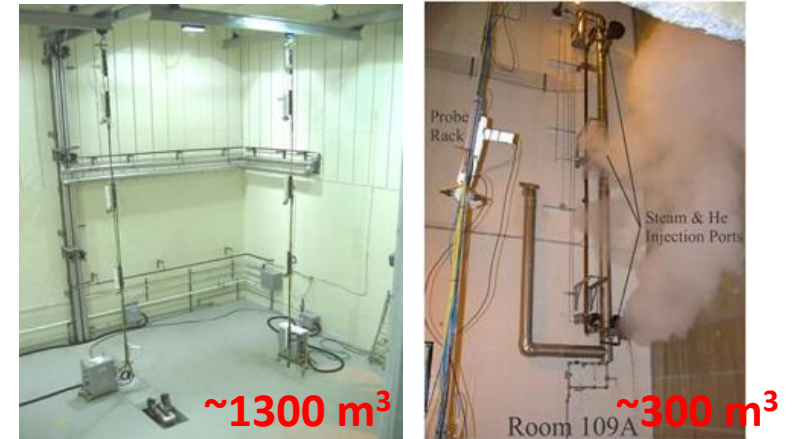


Schematic of TMI-2 Reactor

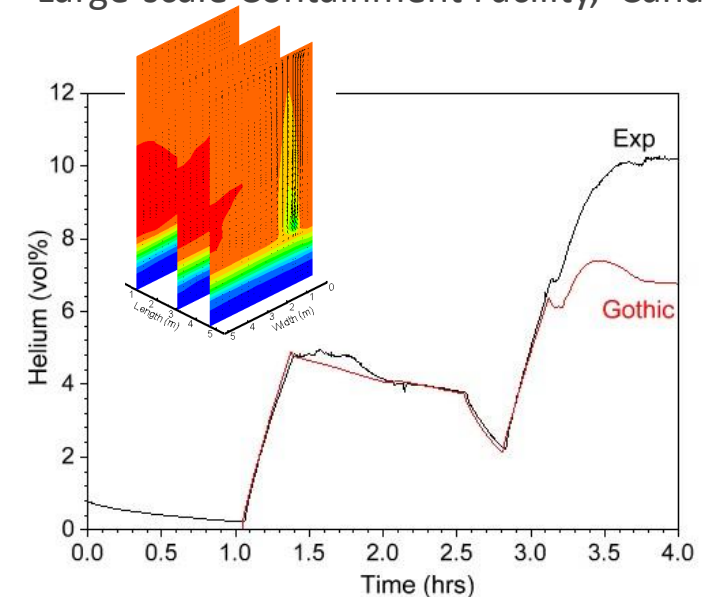
Focus of Nuclear Hydrogen R&D

- **Large-scale experiments**
 - Light gas transport and mixing behavior
 - Hydrogen combustion dynamics in various regimes
 - Mitigation devices qualification/assessment
- **Computer model development and validation**
 - Integral lumped parameter codes (e.g., ASTEC, MAAP, MELCOR, SPECTRA) for system analysis with simple physics and models
 - 3D/CFD codes (e.g., GOTHIC, GASFLOW, Fluent, OpenFOAM) for detailed containment analysis

Ultimate goal is to maintain containment integrity in severe accidents!

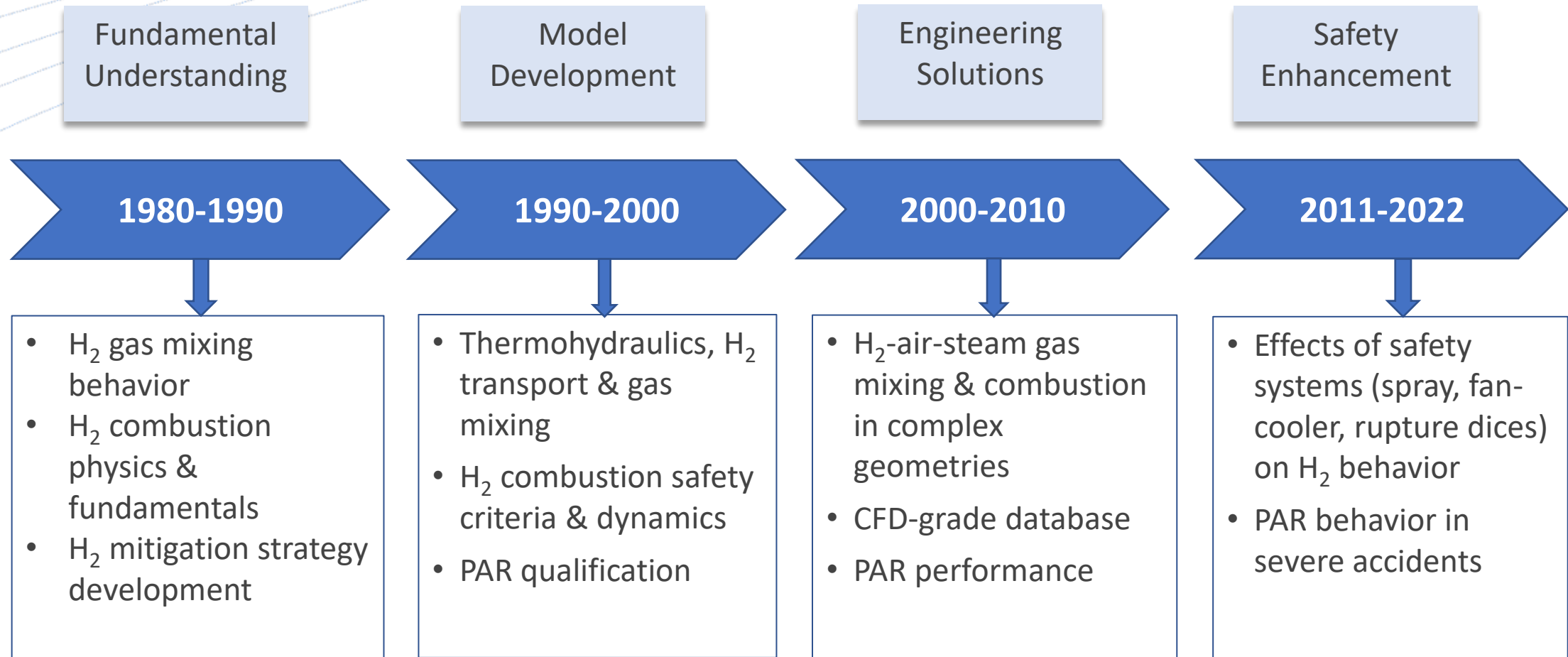


Large-scale Containment Facility, Canada



Z. Liang et al., 19th PBNC, 2014

Evolution of Hydrogen R&D in Nuclear Community



Knowledge Base on Hydrogen Distribution

- **Key phenomena and areas of interest:**

- Turbulence, buoyancy, condensation, natural & forced convection
- Stratification formation and break-up
- Interaction with engineering systems (e.g., air cooler, spray, venting, recombiner)

- **Key parameter – volume Richardson number ^[1]:**

$$Ri_V = g \left(\frac{\rho_{H_2}}{\rho_{air}} - 1 \right) \frac{V_{enclosure}^{1/3}}{U_{H_2}^2}$$

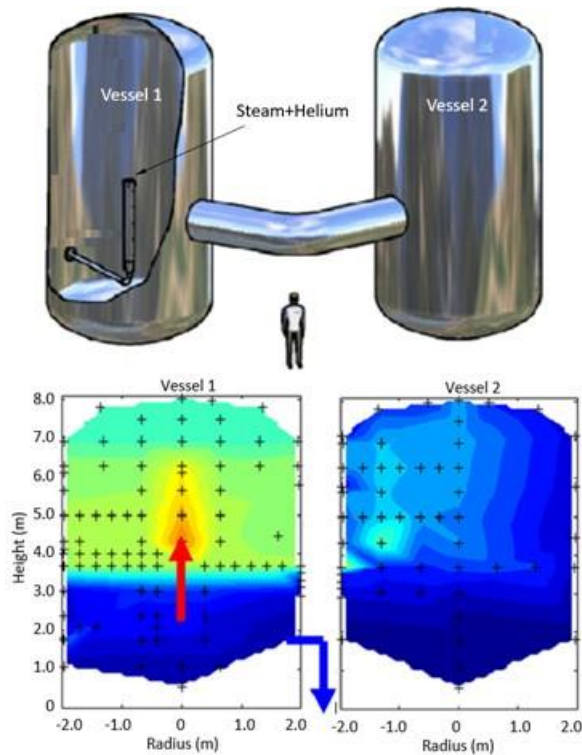
- **Status of knowledge:**

- Numerous light gas mixing tests exist in various scales^[2]; recent research is directed to provide “3D” data for validation of 3D/CFD codes
- Considerable stratification with local high hydrogen concentration remains a concern
- Effectiveness of engineering systems and potential negative impacts on gas mixing (e.g., reducing steam inertisation of the atmosphere) have been studied

[1] R. P. Cleaver, J. Hazard. Mater, 36, 1994, [2] NEA/CSNI/R(99)16

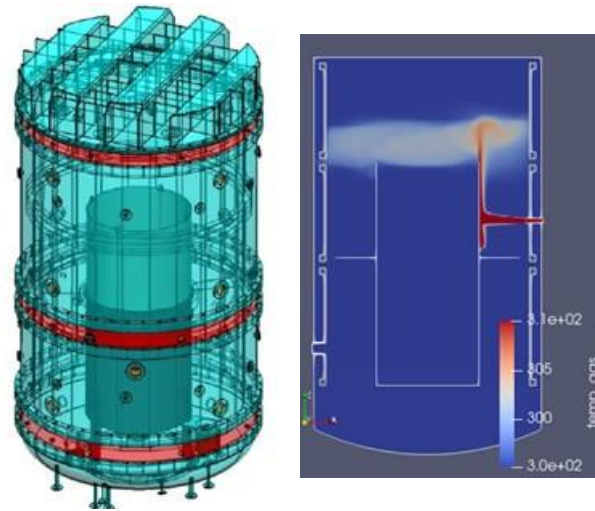
Hydrogen Gas Mixing Facilities and Benchmarks

PANDA (4 interconnected vessels)
90 m³ each, H=4 m, D=4 m
PSI – Switzerland, 1995



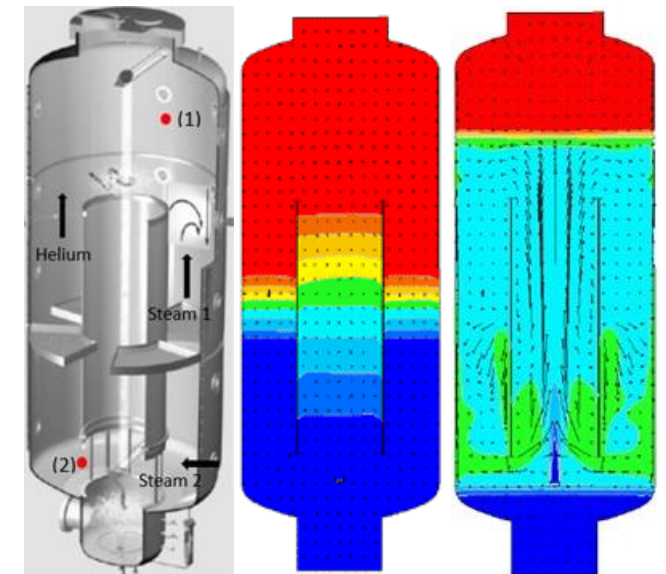
OECD/NEA SETH project [1]

MISTRA (2 nested vessel)
100 m³, H=7.4 m, D=4.2 m
CEA – France, 1999



OECD/NEA HYMERS project [2]

THAI (1 or 2 regions)
60 m³, H=9.2 m, D=3.2 m
BT – Germany, 2000



Fluent simulation

OECD/NEA THAI project – stratification and erosion of light gas [3]

[1] D. Paladino et al., Nucl. Eng. Des., 240 (2), 2010

[2] E. Studer et al., NUTHOS-12, 2018

[3] H.J. Allelein et al., NEA/CSNI/R(2007)10, 2007



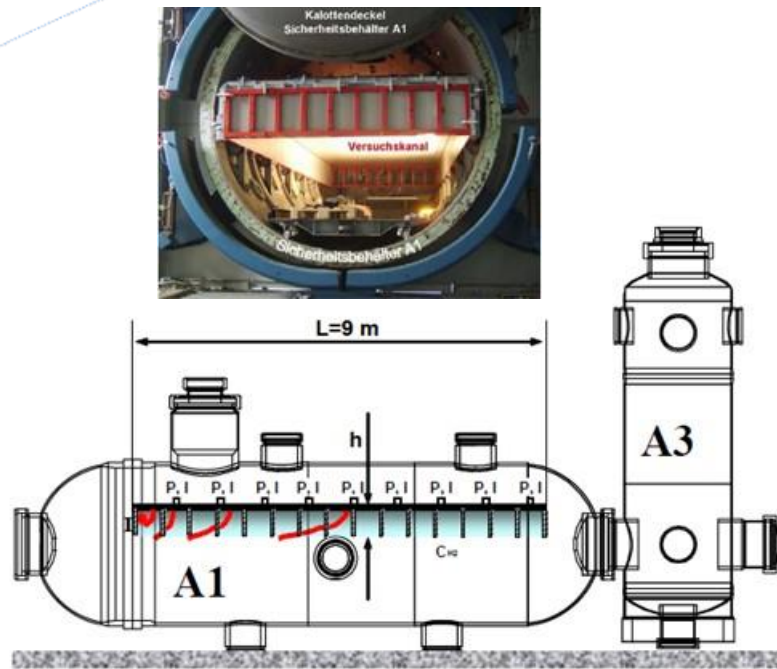
Knowledge Base on Hydrogen Combustion

- **Key phenomena and areas of interest:**
 - Flammability limits, combustion regimes, flame instabilities
 - Laminar/turbulent flame speeds, thermodynamic and kinetic properties
- **Key parameters:**
 - Laminar/turbulent burning velocity, flame thickness, criterion for flame acceleration and deflagration-to-detonation transition (DDT)
- **Status of knowledge:**
 - Early studies in the 80's and 90's established a foundation for development of flame acceleration and DDT criteria^[1]
 - Recent studies are mainly motivated to provide new data for model development and code validation (e.g., ISP49^[2])
 - Critical parameters for non-homogeneous mixtures and interaction with engineering systems (e.g., spray) have been studied^[3]

[1] NEA/CSNI/R(2000)7, [2] NEA/CSNI/R(2011)9, [3] [Home - AMHYCO](#)

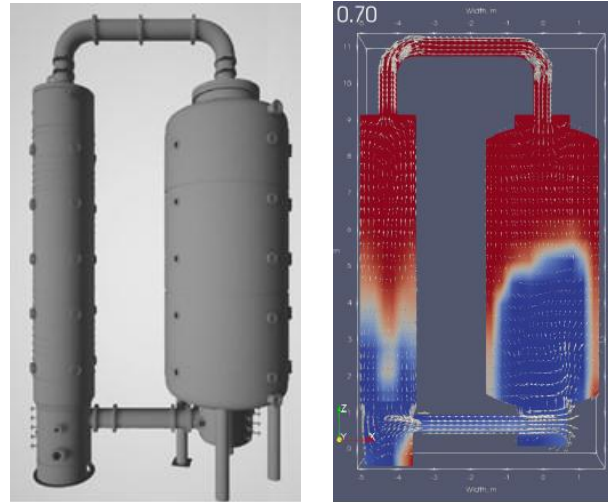
Hydrogen Combustion Facilities and Benchmarks

Large-scale interconnected vessels
110/30 m³, 100/60 bar
KIT – Germany, 2010



Combustion in Semi-Confined Flat Layer [1]

THAI+ (2 vessels), 14 bar
18/60 m³, H=9.2 m, D=1.5/3.2 m
BT – Germany, 2015



GOthic simulation

OECD/NEA THAI3 project – combustion
in interconnected vessels [2]

[1] M. Kuznetsov et al., Nucl. Eng. Des., 286, 2015

[2] S. Gupta et al., Front. Energy 15, 2021

[3] A. Bentaib et al., NURETH-19, 2022

ENACCEF2, H=7.7 m, D=0.23 m, 240 bar
ICARE CNRS – France, 2016



ETSON-SAMHYCO-NET project –
flame acceleration & DDT [3]

Hydrogen Management for NPPs

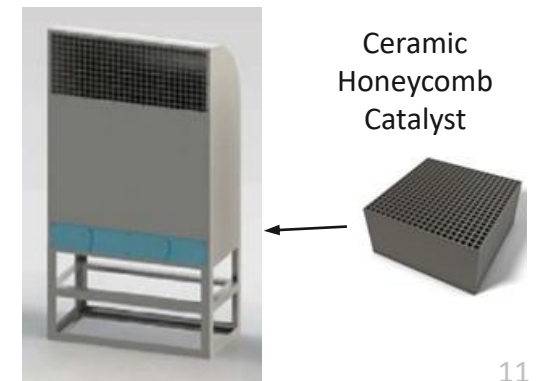
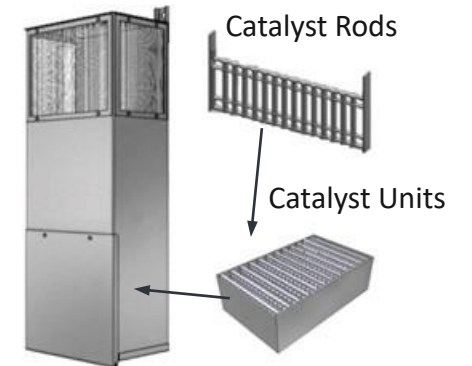
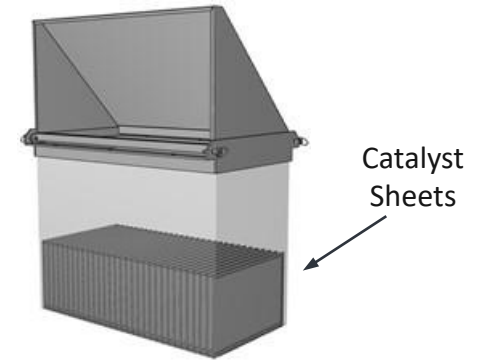
- **Regulations for hydrogen management:**
 - Prevent uncontrolled releases and dispersion of nuclear substances
 - Limit the consequences of an accident
- **General accident management strategies** ^[1]:
 - **Step 1:** reduce the possibility of hydrogen accumulation to flammable concentrations
 - **Step 2:** minimize the volume of gas at flammable concentrations if flammable concentrations cannot be precluded
 - **Step 3:** prevent further increasing hydrogen levels from the flammable to detonable mixture concentrations

[1] NEA/CSNI/R(96)9

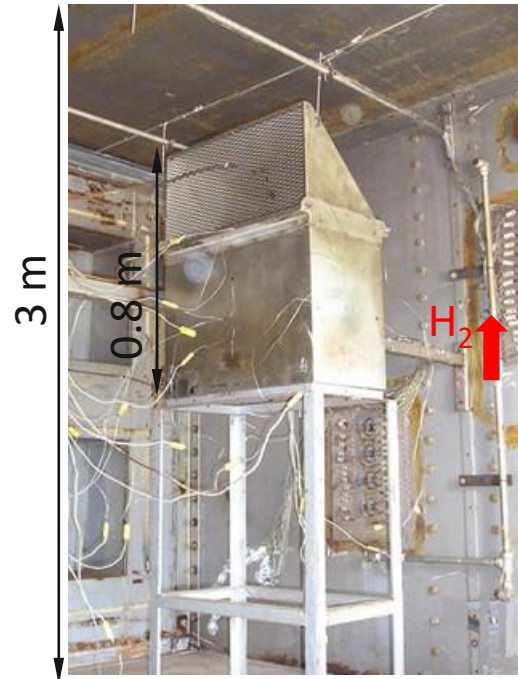
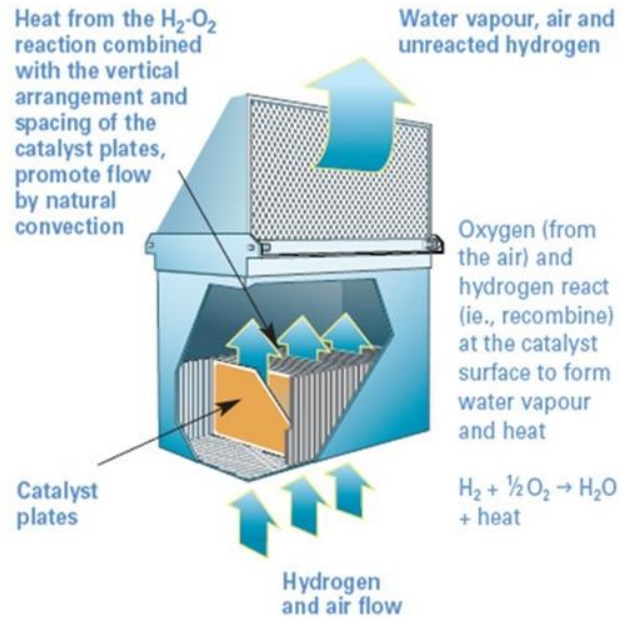


Mitigation Measures Implemented in NPPs

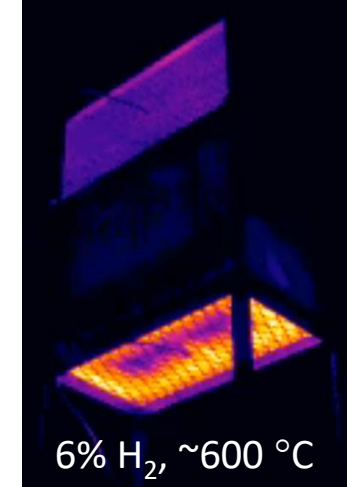
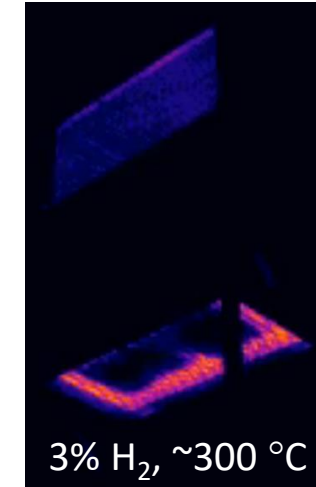
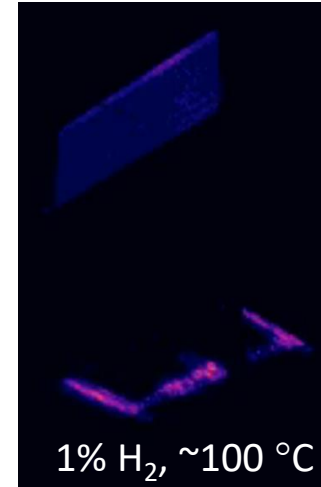
- **Common hydrogen mitigation measures:**
 - Deliberate ignition, consumption/recombination of H₂, replacement of O₂ by inert gas, atmosphere dilution, filtered containment venting
- **Igniter**
 - Prevent “damaging burns” by ignition at near lean flammability limits
 - Can handle higher H₂ flow rates, need to be appropriately located, need external power
- **Passive Autocatalytic Recombiner (PAR)**
 - Self-start/stop, no need for external power
 - Subject to mass transfer limitations and may cause ignition at 6-7% H₂ in air



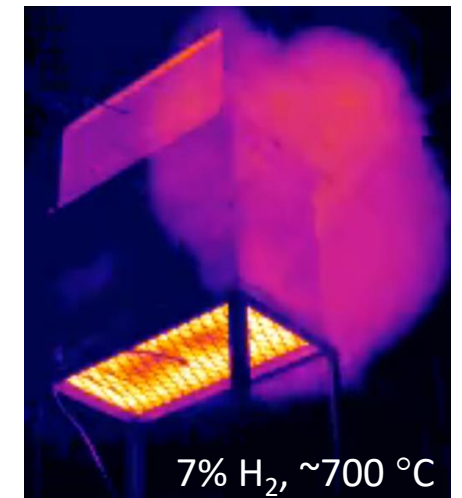
Passive Autocatalytic Recombiner (PAR)



20 x 30 cm
catalyst sheet



- H_2 release rate \gg PAR recombination rate \rightarrow ignition at $\sim 7\% H_2$
- Ignition at extremely lean mixtures: **Good or Bad?**



PAR Testing Facilities and Benchmarks

REKO Facilities, Juelich – Germany



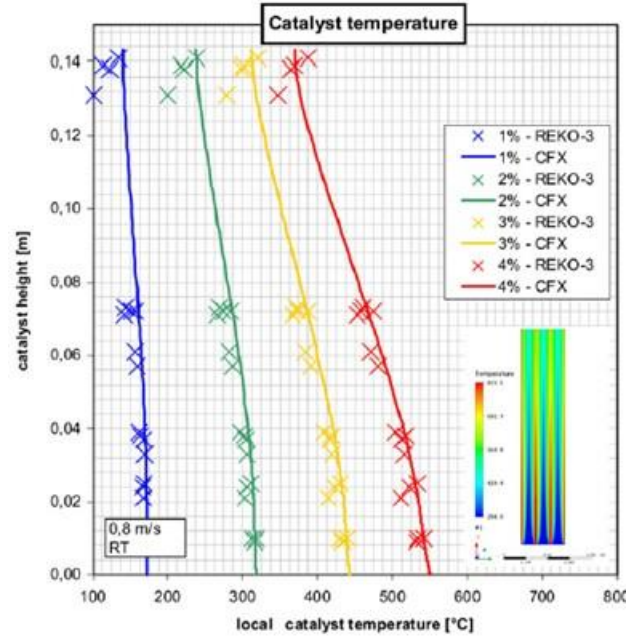
REKO-3

Forced flow, well-defined, steady-state, catalyst sample

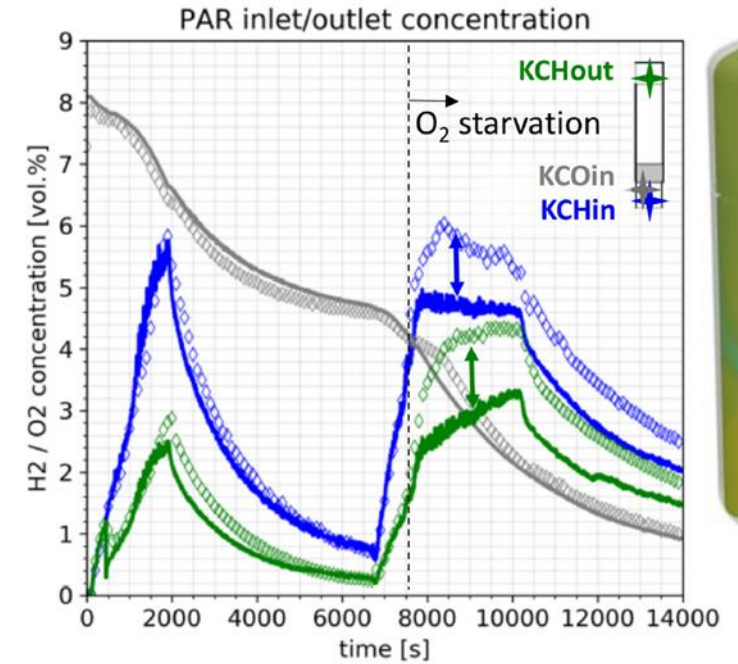


REKO-4

Pressure vessel 5.3 m³, H=4 m, D=1.4 m full-size PAR



Coupling of a 2D mechanistic PAR model with CFD code [1]



Validation of containmentFOAM using large-scale PAR tests conducted in THAI facility [2]

THAI



Open Questions and Linkage with Other Industries

- **Scaling effects**
 - Height of test facilities: 8-10 m, an order of magnitude smaller than nuclear containments
- **Safety criterion & combustion behavior**
 - Slow flame, fast flame, DDT
 - Non-homogeneous/stratified mixtures, unconfined mixtures
 - Complex geometry, multi-connected rooms
 - Interaction with mitigation systems (e.g., spray, venting)
- **Computer codes**
 - Uncertainty/accuracy, user effects, applicable ranges, validation
- **Coupling or co-locating** of a nuclear reactor with hydrogen production installations

Questions?

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