

lear | Laboratoires Nucléaires | Canadiens

Application of Passive Autocatalytic Recombiners (PARs) for Hydrogen Mitigation: 2D Numerical Modeling and Experimental Validation

ICHS Conference, Quebec City, QC

Marco A. B. Zanoni Research Scientist Hydrogen Technologies Branch marco.bazelattozanoni@cnl.ca

2023 September 19

Canadian Nuclear | Laboratoires Nucléaires Laboratories | Canadiens

OFFICIAL USE ONLY / À USAGE EXCLUSIF



Background: Hydrogen Release

Nuclear Context:

- Hydrogen (H₂) and carbon monoxide (CO) can be released during a nuclear reactor accident with a loss of coolant:
 - H₂: Hot steam + Zr metal
 - H₂+CO: Molten core concrete interaction

Non-Nuclear Context:

H₂ can be released from leaks in H₂ vehicles placed in confined and semi-confined areas: underground mining, parking garages, and road tunnels where CO can be present.





Huang, T., et al., Modeling of hydrogen dispersion from hydrogen fuel cell vehicles in an underground parking garage. International Journal of Hydrogen Energy, 2022. 47(1): p. 686-696.



Canadian Nuclear | Laboratoires Nucléaires Laboratories | Canadiens

OFFICIAL USE ONLY / À USAGE EXCLUSIF

Hydrogen Mitigation

Both Contexts:

- Hydrogen accumulation could create a flammable mixture:
 - Ignition \rightarrow Fire/explosion:

 \rightarrow threat to structures and life.

Hydrogen Mitigation Measures

- ≻ Large free volume → dilution of $H_{2.}$
- Ventilation (non-nuclear context).
- Active or Passive Autocatalytic Recombiners.





Catalyst Plate





PAR Operation

Thermochemical Mechanisms:

- Species transport from the bulk fluid to the catalyst surface.
- Surface reactions.
- Convection of the bulk fluid through the PAR chimney.
- Heat losses through convection and radiation.
- Catalyst poisoning (if CO is available).

• Experiments:

- Limited in capturing complex mechanisms.
- Potentially expensive and time consuming.
- Numerical Model:
 - Used to improve the fundamental understanding of such complex mechanisms.
 - Predict the PAR performance in a wide range of conditions.



Kelm, S., W. Jahn, and E.-A. Reinecke. Operational behaviour of catalytic recombiners - experimental results and modelling approaches. in Computational Fluid Dynamics (CFD) in Nuclear Reactor Safety (NRS) -Proceedings of the workshop on Experiments and CFD Code Application to Nuclear Reactor Safety (XCFD4NRS). 2008. Nuclear Energy Agency of the OECD (NEA).



2D Transient PAR Model: Experimental Setup

REKO-3 Tests (JÜLICH, Germany)

- H₂-CO steady-state tests.
- Forced flow.
- Different H₂ and CO inlet concentrations.
- Catalyst temperature measurements.
- Gas concentration measurements (inlet and outlet).





2D Transient PAR Model: Model Geometry



2D Transient PAR Model: Governing Mechanisms



Model Physics

- Forced Laminar flow
- Heat transfer in solids and fluid
- Radiation heat losses
- Transport of species (H₂, O₂, N₂, H₂O, CO, CO₂)
- Surface reactions:

$$\begin{array}{l} k_{H_2}^f \\ H_2 \rightleftharpoons H_{2(ads)} \\ k_{H_2}^r \\ k_{H_2}^f \\ 0_2 \rightleftharpoons 0_{2(ads)} \\ k_{0_2}^r \end{array} 2 H_{2(ads)} + O_{2(ads)} \xrightarrow{k_{H_2-O_2}} 2 H_2 O_{(v)} \\ 2 H_{2(ads)} + O_{2(ads)} \xrightarrow{k_{H_2-O_2}} 2 H_2 O_{(v)} \\ 2 H_{2(ads)} + O_{2(ads)} \xrightarrow{k_{H_2-O_2}} 2 H_2 O_{(v)} \\ 2 H_2(ads) + O_{2(ads)} \xrightarrow{k_{H_2-O_2}} 2 H_2 O_{(v)} \\ 2 H_2(ads) + O_{2(ads)} \xrightarrow{k_{H_2-O_2}} 2 H_2 O_{(v)} \\ 2 H_2(ads) + O_{2(ads)} \xrightarrow{k_{H_2-O_2}} 2 H_2 O_{(v)} \\ 2 H_2(ads) + O_{2(ads)} \xrightarrow{k_{H_2-O_2}} 2 H_2 O_{(v)} \\ 2 H_2(ads) + O_{2(ads)} \xrightarrow{k_{H_2-O_2}} 2 H_2 O_{(v)} \\ 2 H_2(ads) + O_{2(ads)} \xrightarrow{k_{H_2-O_2}} 2 H_2 O_{(v)} \\ 2 H_2(ads) + O_{2(ads)} \xrightarrow{k_{H_2-O_2}} 2 H_2 O_{(v)} \\ 2 H_2(ads) + O_{2(ads)} \xrightarrow{k_{H_2-O_2}} 2 H_2 O_{(v)} \\ 2 H_2(ads) + O_{2(ads)} \xrightarrow{k_{H_2-O_2}} 2 H_2 O_{(v)} \\ 2 H_2(ads) + O_{2(ads)} \xrightarrow{k_{H_2-O_2}} 2 H_2 O_{(v)} \\ 2 H_2(ads) + O_{2(ads)} \xrightarrow{k_{H_2-O_2}} 2 H_2 O_{(v)} \\ 2 H_2(ads) + O_{2(ads)} \xrightarrow{k_{H_2-O_2}} 2 H_2 O_{(v)} \\ 2 H_2(ads) + O_{2(ads)} \xrightarrow{k_{H_2-O_2}} 2 H_2 O_{(v)} \\ 2 H_2(ads) + O_{2(ads)} \xrightarrow{k_{H_2-O_2}} 2 H_2 O_{(v)} \\ 2 H_2(ads) + O_{2(ads)} \xrightarrow{k_{H_2-O_2}} 2 H_2 O_{(v)} \\ 2 H_2(ads) + O_{2(ads)} \xrightarrow{k_{H_2-O_2}} 2 H_2 O_{(v)} \\ 2 H_2(ads) + O_{2(ads)} \xrightarrow{k_{H_2-O_2}} 2 H_2 O_{(v)} \\ 2 H_2(ads) + O_{2(ads)} \xrightarrow{k_{H_2-O_2}} 2 H_2 O_{(v)} \\ 2 H_2(ads) + O_{2(ads)} \xrightarrow{k_{H_2-O_2}} 2 H_2 O_{(v)} \\ 2 H_2(ads) + O_{2(ads)} \xrightarrow{k_{H_2-O_2}} 2 H_2 O_{(v)} \\ 2 H_2(ads) + O_{2(ads)} \xrightarrow{k_{H_2-O_2}} 2 H_2 O_{(v)} \\ 2 H_2(ads) + O_{2(ads)} \xrightarrow{k_{H_2-O_2}} 2 H_2 O_{(v)} \\ 2 H_2(ads) + O_{2(ads)} \xrightarrow{k_{H_2-O_2}} 2 H_2 O_{2(ads)} \\ 2 H_2(ads) + O_{2(ads)} \xrightarrow{k_{H_2-O_2}} 2 H_2 O_{2(ads)} \\ 2 H_2(ads) + O_{2(ads)} \xrightarrow{k_{H_2-O_2}} 2 H_2 O_{2(ads)} \\ 2 H_2(ads) + O_{2(ads)} \xrightarrow{k_{H_2-O_2}} 2 H_2 O_{2(ads)} \\ 2 H_2(ads) + O_{2(ads)} \xrightarrow{k_{H_2-O_2}} 2 H_2 O_{2(ads)} \\ 2 H_2(ads) + O_{2(ads)} \xrightarrow{k_{H_2-O_2}} 2 H_2 O_{2(ads)} \\ 2 H_2(ads) + O_{2(ads)} \xrightarrow{k_{H_2-O_2}} 2 H_2 O_{2(ads)} \\ 2 H_2(ads) + O_{2(ads)} \xrightarrow{k_{H_2-O_2}} 2 H_2 O_{2(ads)} \\ 2 H_2(ads) + O_{2(ads)} \xrightarrow{k_{H_2-O_2}} 2 H_2 O_{2(ads)} \\ 2 H_2(ads) + O_{2(ads)} \xrightarrow{k_{H_2-O_2}} 2 H_2 O_{2$$

 k_{CO}^r

2D Transient PAR Model: REKO-3 Experiments

Experiment (#)	Forced Inlet Velocity (m/s)	H _{2,in} (vol.%)	CO _{in} (vol.%)
1	1.0	4.0	0.0
2	1.0	4.0	1.0
3	1.0	4.0	2.0



> H₂-O₂ Calibration

- > CO-O₂ Calibration
- > Model Validation



2D Transient PAR Model: Experiments



2D Transient PAR Model: Calibration



2D Transient PAR Model: Validation



- Plate base: higher temperatures
 - Higher H₂ concentrations
- Plate top: lower temperatures
 - Lower H₂ concentrations
 - Heat losses
- Model reproduces well experimental data
- Model reproduces well experiments at different conditions

2D Transient PAR Model: Contour Profiles (H_{2,in}=4%, V_{in}=1 m/s, CO_{in}=2%)



- Temperatures: Higher at the catalyst plate,
- lower at the channel.
- H₂: Entirely recombined.
- **CO:** Not entirely recombined.
- **O**₂: in excess (no O₂ limitations)

2D Transient PAR Model: Catalyst Surface Properties

 θ_i = Fractional surface coverages. Γ_s = density of sites of the surface. σ_i = site occupancy number. $c_{s,i}$ = surface concentrations.

$$\theta_{free} = 1 - \sum_{i} \theta_{i}$$

 θ_{free} = fraction of free sites on the surface.





 $\theta_i = \frac{\sigma_i c_{s,i}}{\Gamma_s}$

2D Transient PAR Model: Example of Poisoning

- CO Poisoning (Note: CO was only used as an example!! In reality, this might be different)
- Site occupancy number (σ) was manually increased





2D Transient PAR Model: Example of Poisoning





2D Transient PAR Model: Example of Poisoning







- H₂ and CO recombination reactions were tested in a 2D transient CFD model to simulate PAR performance.
- The model matched experimental catalyst temperature well along different conditions.
- > Surface properties were simulated as a new feature in the model.
- > Catalyst poisoning was tested showing that the model can handle such scenarios.
- Altogether, the model shows how surface chemistry can be used as tool to explain interesting mechanisms that cannot be easily seen in experiments.



OFFICIAL USE ONLY / À USAGE EXCLUSIF

Questions?

Marco A. B. Zanoni, PhD Research Scientist Hydrogen Technologies Branch marco.bazelattozanoni@cnl.ca



OFFICIAL USE ONLY / À USAGE EXCLUSIF