

# EFFECTS OF RENEWABLE ENERGY UNSTABLE SOURCE TO HYDROGEN PRODUCTION: SAFETY CONSIDERATIONS

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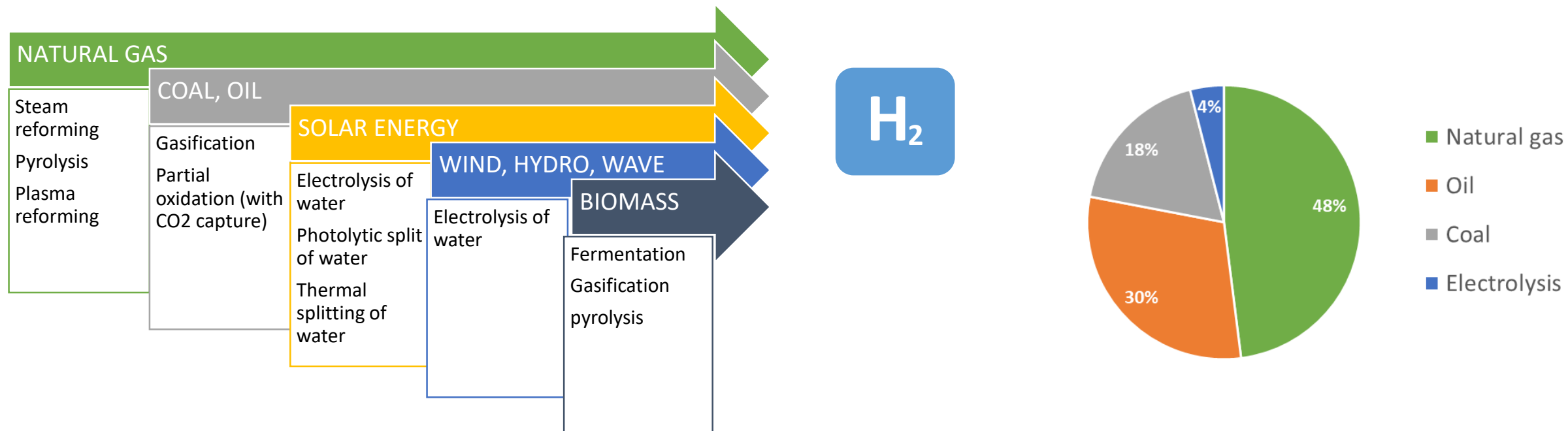
The Scottish Government and IA HySafe invite you to the unique

**INTERNATIONAL CONFERENCE ON HYDROGEN  
SAFETY 2021**

**"Safe Hydrogen for Net Zero"**

**Edinburgh on 21-24 September 2021**

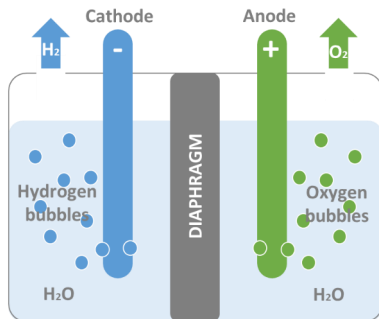
# Hydrogen production - electrolysis



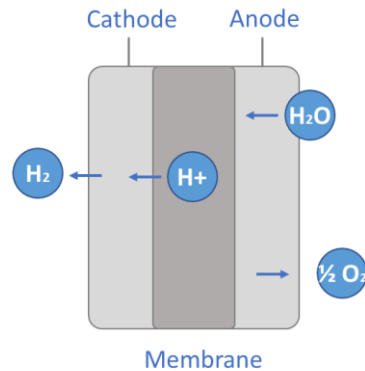
- Water electrolysis is a key technology for splitting water into hydrogen and oxygen by using renewable energy
- Solar and wind energy
  - the most widespread distribution
  - particular advantages, since the exceeding electrical energy produced can be stored in hydrogen, balancing the discrepancy between energy demand and production
- The main issue with the use of renewable energy is the unsteady distributed and intermittent local availability

# Type of electrolysis

## Alkaline water electrolysis (AEL)

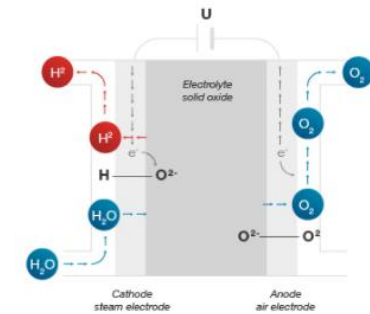


## Proton exchange membrane electrolysis (PEM)



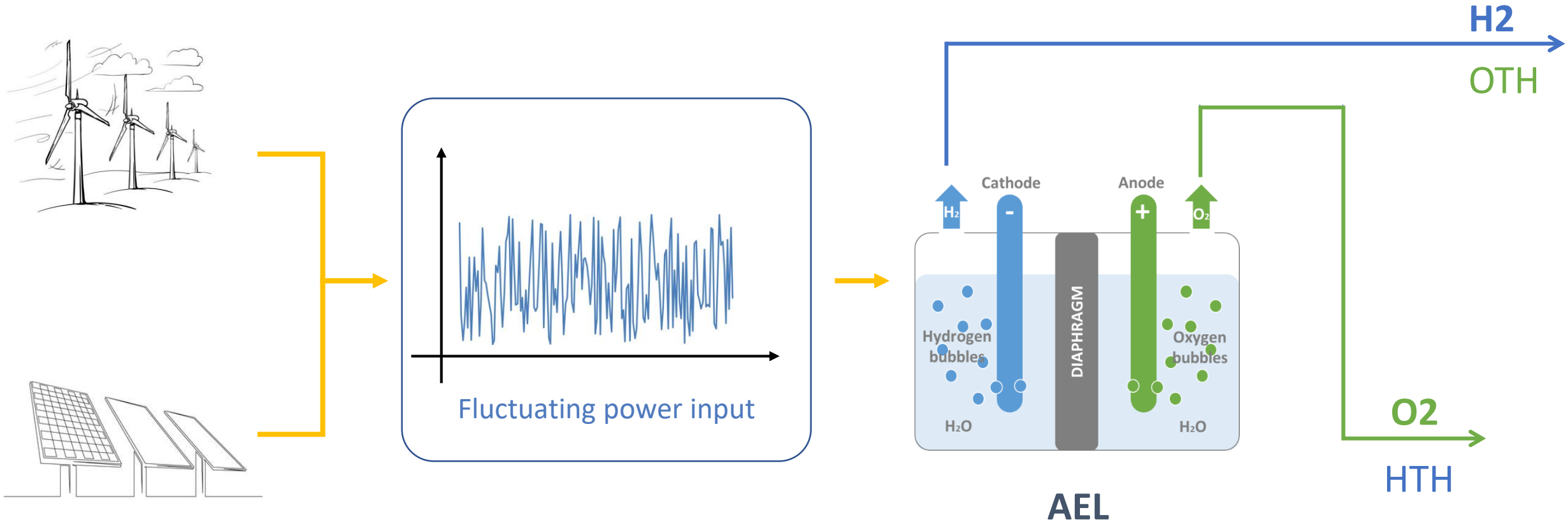
Low temperature

## Solid oxide electrolysis (SOEL)



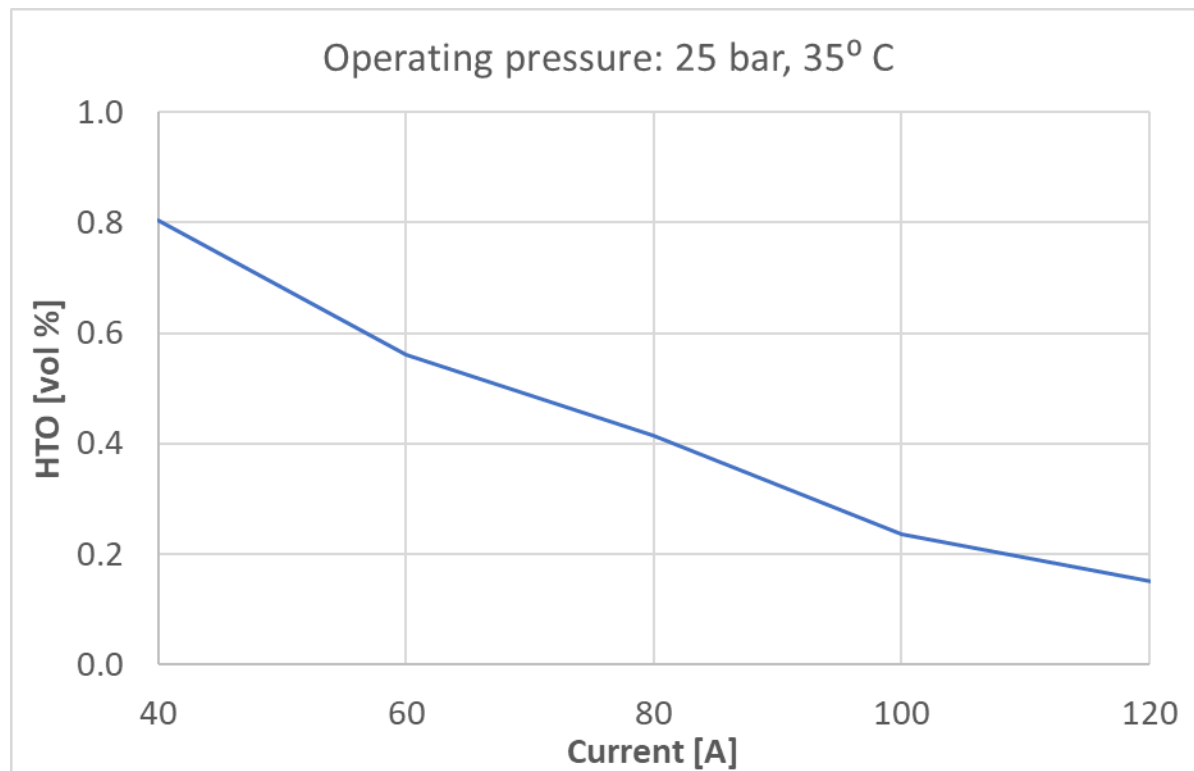
High temperature

# Electrolyser + fluctuating power input



# HTO: amount of hydrogen in oxygen

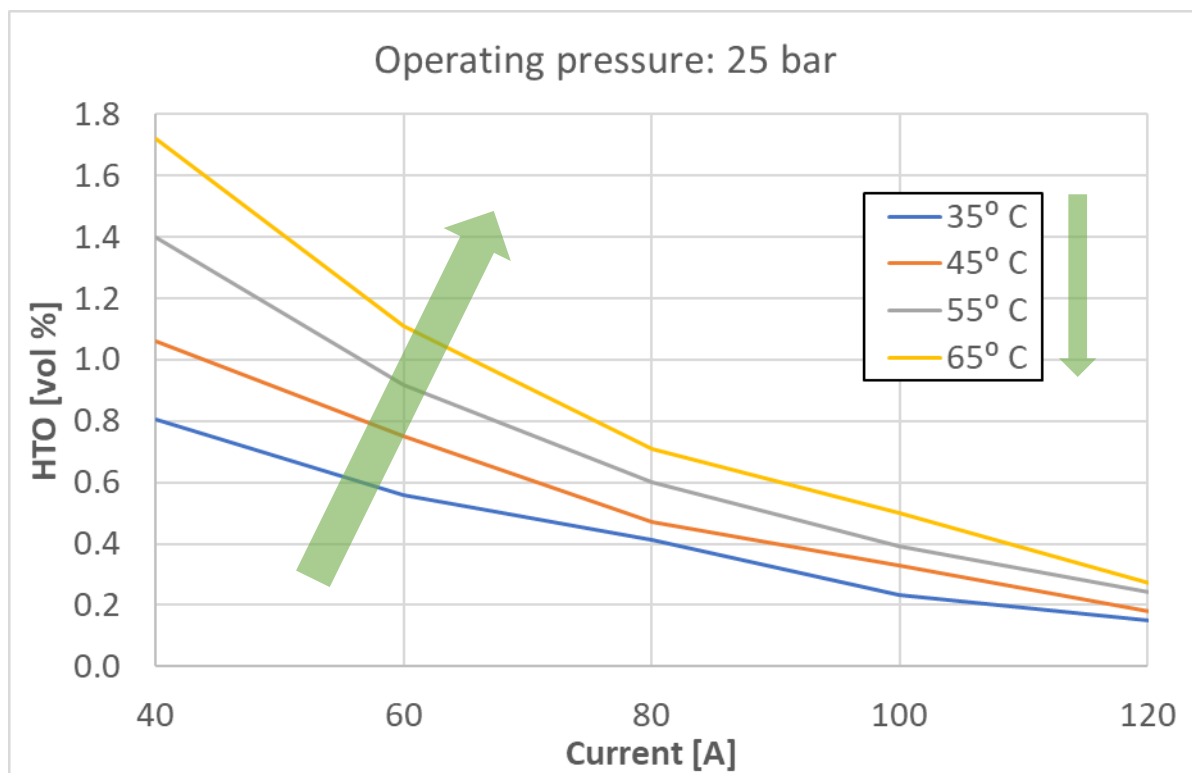
Increase in HTO as the current decreases:



- H<sub>2</sub> molecules produced at the electrodes join up more slowly to form bubbles
  - the molecules are held inside the cell for a longer period of time
  - thereby contributing to the increase in the hydrogen diffusion rate through the diaphragms
- HTO trend is exponential with the decrease in current
  - associated with a considerable decrease in the production of hydrogen at low currents due to the parasitic currents through the electrolyser stack

Alkaline water electrolysis

# HTO in relation with temperature

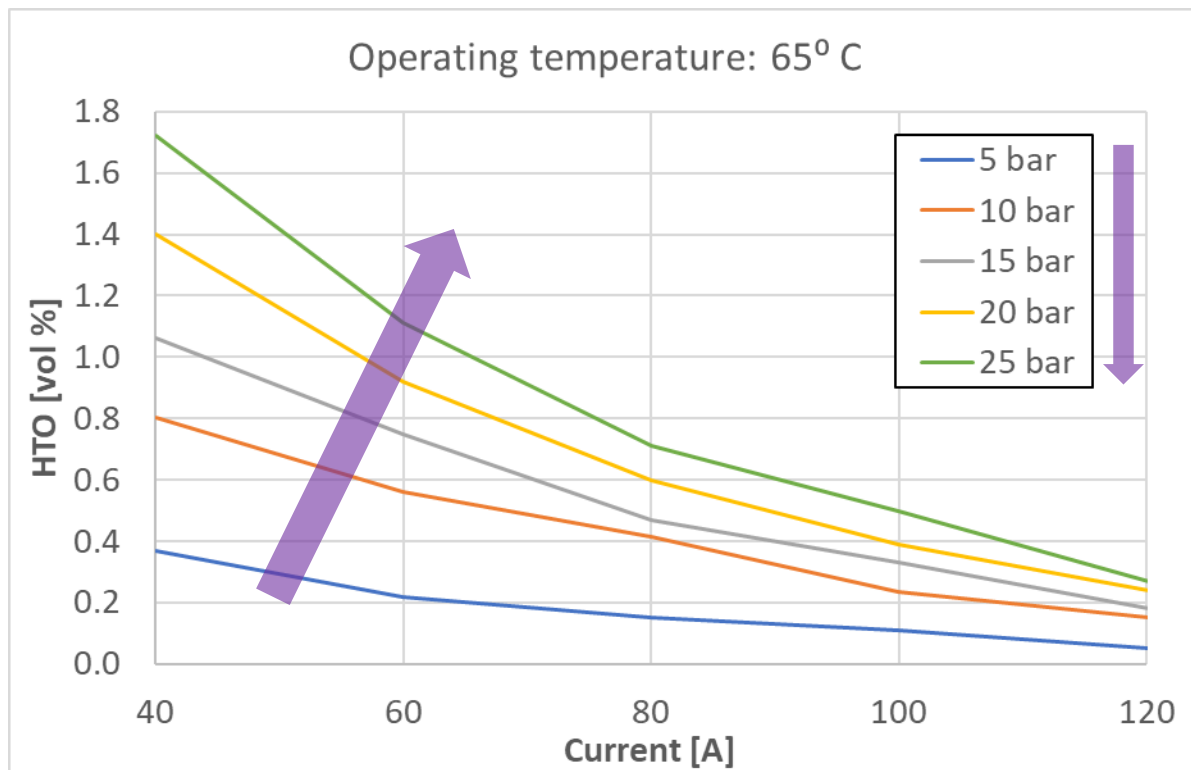


## Increase in HTO as the temperature increases

- Quasi-linear trend for each current
- The temperature increase in the electrolysis stack leads to an increase in the diffusion rate for the small gas bubbles through the diaphragms
- When the process temperature increases, the thermal energy available in the system also increases and the particles, including the gases, increase their mobility.

At 120 A current, the HTO is 80% greater at 65° C (0.27 vol.%) compared to 35° C (0.15 vol.%)

# HTO in relation with pressure



## Increase in HTO as the pressure increases

- HTO level increases quasi-proportionally
- The higher is the pressure, the lower is the volume of the gas bubbles generated in the electrolysis
  - This decrease in the size of the bubbles leads to a greater migration of hydrogen through the electrolyte pathways and diaphragm pores

At 5 bar, the HTO value for 40 A is 0.36 vol.%, whilst for a pressure of 25 bar and the same current level, it is approximately 4.8 times greater, that is 1.72 vol.%

# HTO vs. OTH

- OTH trends with current, temperature and pressure are equivalent to the HTO
- HTO is 10-30 times greater than the OTH (for small size alkaline electrolyzers HTO is usually 3-7 times greater than the OTH)
  - the hydrogen molecules, in addition to being lighter than the other elements, are also smaller and therefore have a greater fugacity and diffusivity through the electrolyte pathways and stack cell diaphragms, compared to oxygen.
- The best operating conditions to minimize HTO and OTH are basically those in which the electrolyser is operating at a low pressures and high currents
- The experiments confirm the lower is the pressure level, the lower is the gas impurities



# Safety and technical regulations

- All the devices relevant for hydrogen production must to be complied with **ATEX directives**
  - the essential health and safety requirements and conformity assessment procedures, **to be applied before products are placed on the EU market**
  - covers equipment and protective systems intended for use in potentially explosive atmospheres (mixture of air with dangerous substances in the form of gases, vapor, mist or dust)
- The relevant Standard document is the **ISO 22734** (Hydrogen generators using **water electrolysis**)
  - defines the construction, safety, and performance requirements of modular or factory-matched hydrogen gas generators, using electrochemical reactions to electrolyze water to produce hydrogen
- Fuel Cell and Hydrogen Joint Undertaking (**FCH JU**), with the support of the European Hydrogen Safety Panel (**EHSP**), organized a **workshop focused on the safety aspects of electrolysis technology**
  - A typical cause of fires and explosion in alkaline chlorine electrolysis is the accidental creation and ignition of flammable gaseous mixtures (hydrogen-chlorine, hydrogen-air/oxygen)

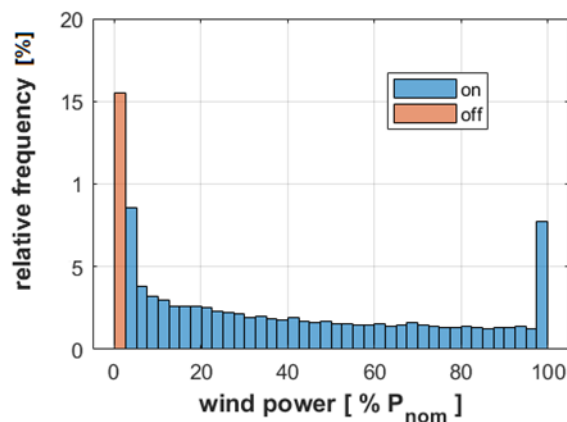
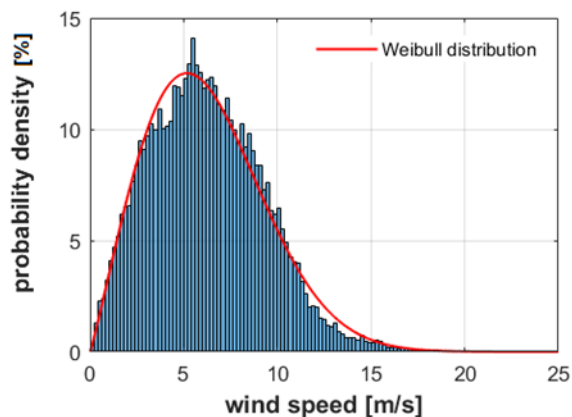
# Safety and technical regulations

- In the recent **accident** (2019) at the alkaline electrolyser in **Gangneung, Korea**, the introduction of hydrogen into the oxygen stream was not **caused by** membrane perforation, but **gases cross-over under low power operating conditions**
  - Such cross-over was not detected and the typical catalytic oxygen removal system was not installed
  - an explosive mixture of hydrogen and oxygen formed in the hydrogen storage containers was ignited by an unknown source



# Renewable power data input

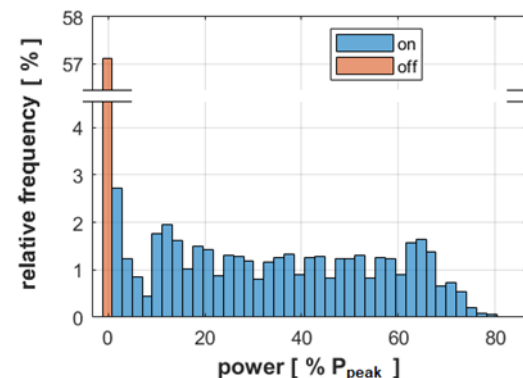
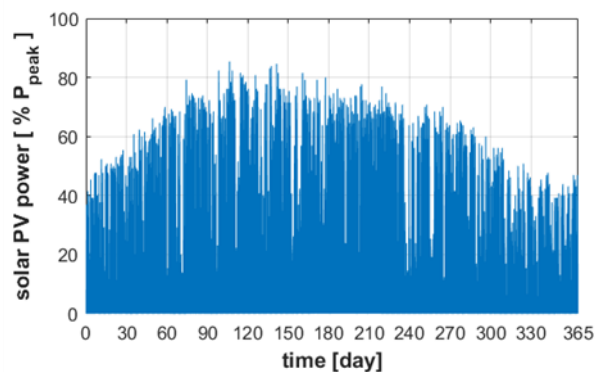
- Wind energy input: variable power data (NREL Wind Prospector web site) series reproducing the renewable power must be given as input to the electrolyser



$$P_{wt} = \begin{cases} 0, & v_w < v_{ci} \text{ or } v_w < v_{co} \\ (a_1 v_w^3 + a_2 v_w^2 + a_3 v_w + a_4) P_{wt,nom}, & v_{ci} \leq v_w \leq v_r \\ P_{wt,nom} & v_r \leq v_w \leq v_{co} \end{cases}$$

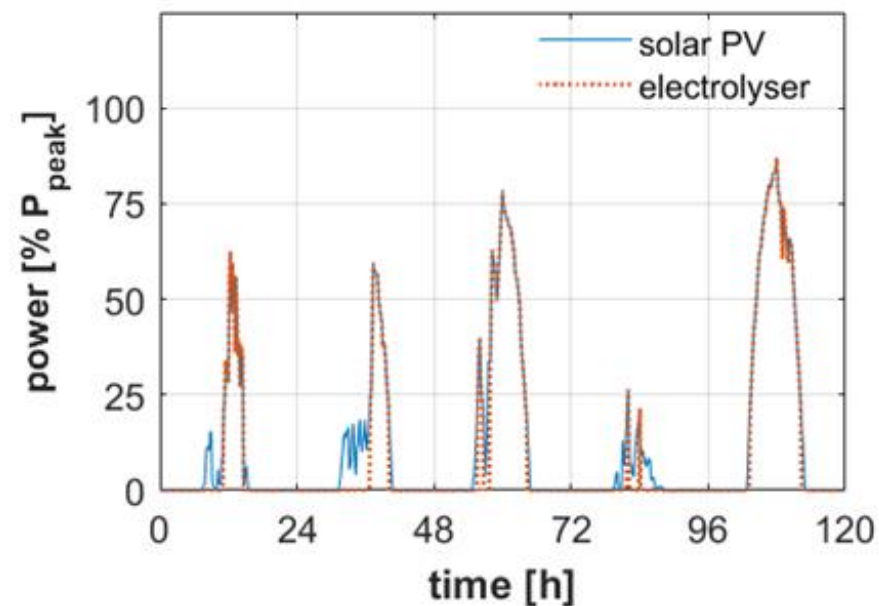
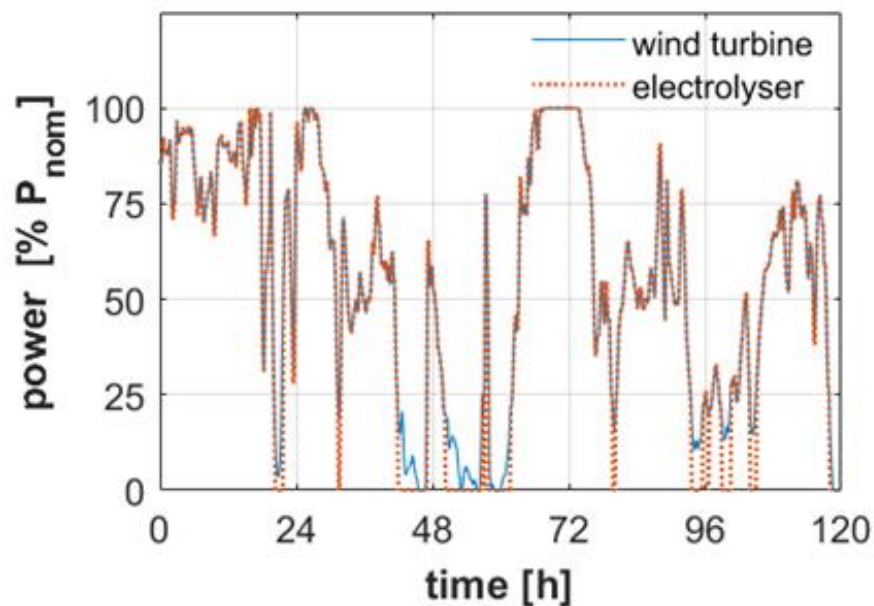
$$a_1 = -2.715 \cdot 10^{-3} \text{ (m/s)}^{-3}, a_2 = 6.138 \cdot 10^{-2} \text{ (m/s)}^{-2}, a_3 = -0.2950 \text{ (m/s)}^{-1}, a_4 = 0.4318$$

- PV input: a site located in the New York state (USA) was chosen since it is characterized by seasonal power variability



# Renewable power data input

- The wind and PV nominal power were set equal to the electrolyser nominal power
- The electrolyser must work in a power range of 20-100% nominal power to avoid safety issues
  - As a result, two electrolyser annual power input profiles were obtained respectively for the cases of wind and solar PV sources
- The electrolyser power input follows the renewable power when possible and it is characterized by a high variability and frequent on-off



# Experimental set-up: hydrogen production

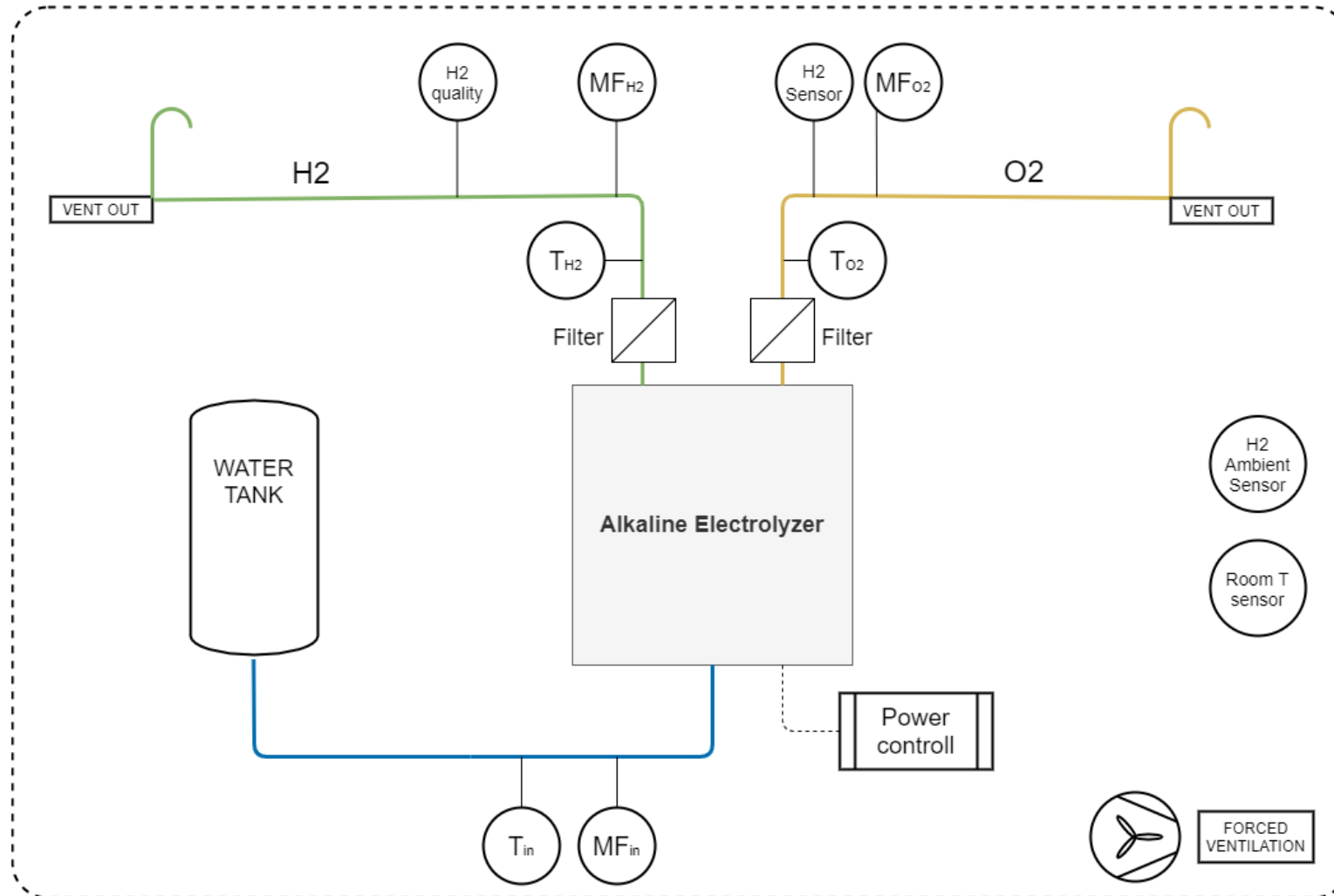


|                            |                        |
|----------------------------|------------------------|
| Installed power            | 35 kW                  |
| Hydrogen production rate   | 4.4 Nm <sup>3</sup> /h |
| Oxygen production rate     | 2.2 Nm <sup>3</sup> /h |
| Hydrogen delivery pressure | 2.0 barg               |
| Hydrogen delivery quality  | 99.5% ± 0.3% dry basis |

# McPhy

- ~ 5.3 kWh of electric energy are required per Nm<sup>3</sup> of H<sub>2</sub> (including energy losses)
- For safety reason, the unit can produce H<sub>2</sub> included in the range 25÷100% of nominal flowrate
- Shutdown procedure when the pressure > 2.5 barg
- Shutdown procedure when the electrolyte (containing H<sub>2</sub>) temperature = 80 °C
- Two additional pressure swithes to stop the system at very high pressure (i.e. 5 barg)
  - two safety valves release hydrogen or oxygen to the dedicated vent lines

# Laboratory layout



# Future experimental activities

- Tests on polarization curve
  - to determine the change in the stack voltage with the variation in the supplied current under steady-state conditions at constant reference temperature and pressure
- The electrolyser will then be tested:
  - under dynamic protocols consisting of potential sweeping with different with short holds to simulate alternating power operation
  - under a variable input power that simulates the renewable power assigned by the power control
- The aim of the tests is to evaluate the effects of the dynamic operation on the hydrogen quality and possible safety issues