



# Lessons Learned from Large Scale H<sub>2</sub> Production Project

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## Shell’s net carbon intensity

Also, in this presentation we may refer to Shell’s “Net Carbon Intensity”, which includes Shell’s carbon emissions from the production of our energy products, our suppliers’ carbon emissions in supplying energy for that production and our customers’ carbon emissions associated with their use of the energy products we sell. Shell only controls its own emissions. The use of the term Shell’s “Net Carbon Intensity” is for convenience only and not intended to suggest these emissions are those of Shell plc or its subsidiaries.

## Shell’s net-zero Emissions Target

Shell’s operating plan, outlook and budgets are forecasted for a ten-year period and are updated every year. They reflect the current economic environment and what we can reasonably expect to see over the next ten years. Accordingly, they reflect our Scope 1, Scope 2 and Net Carbon Intensity (NCI) targets over the next ten years. However, Shell’s operating plans cannot reflect our 2050 net-zero emissions target and 2035 NCI target, as these targets are currently outside our planning period. In the future, as society moves towards net-zero emissions, we expect Shell’s operating plans to reflect this movement. However, if society is not net zero in 2050, as of today, there would be significant risk that Shell may not meet this target.

## Forward Looking Non-GAAP measures

This presentation may contain certain forward-looking non-GAAP measures such as cash capital expenditure and divestments. We are unable to provide a reconciliation of these forward-looking Non-GAAP measures to the most comparable GAAP financial measures because certain information needed to reconcile those Non-GAAP measures to the most comparable GAAP financial measures is dependent on future events some of which are outside the control of Shell, such as oil and gas prices, interest rates and exchange rates. Moreover, estimating such GAAP measures with the required precision necessary to provide a meaningful reconciliation is extremely difficult and could not be accomplished without unreasonable effort. Non-GAAP measures in respect of future periods which cannot be reconciled to the most comparable GAAP financial measure are calculated in a manner which is consistent with the accounting policies applied in Shell plc’s consolidated financial statements.

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# Project: Holland Hydrogen 1

## TIMELINE

2020



Project  
Initiation

2021



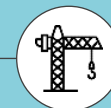
Vendor select  
& DG3

June 2022



Final  
Investment  
Decision

2023

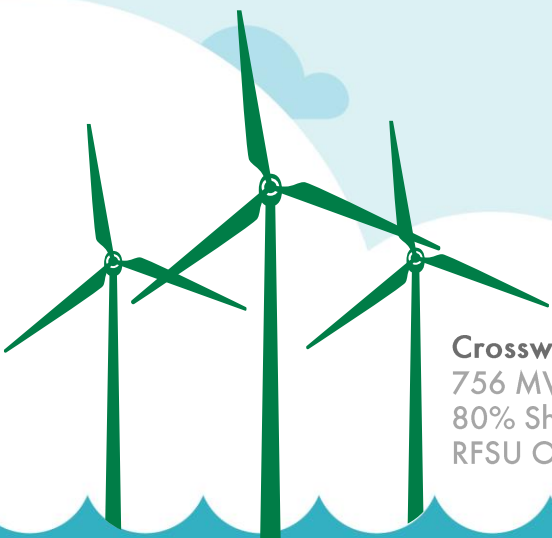


HH1  
Construction,  
HKN online

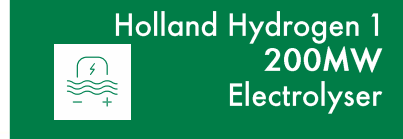
2025



Commissioning  
and H<sub>2</sub> supply

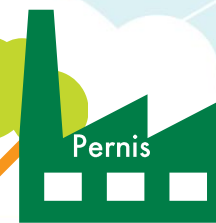


**Crosswind**  
756 MW capacity  
80% Shell Share  
RFSU Oct 2023



Holland Hydrogen 1  
200MW  
Electrolyser

Peak production: 80 t/pd  
Annual production: 20 ktpa



Daily use: 550 tpd  
Flexible production



Mobility platform  
~ 2300 trucks

**Future use:**  
Marine (RED III)  
Industry (RED III)



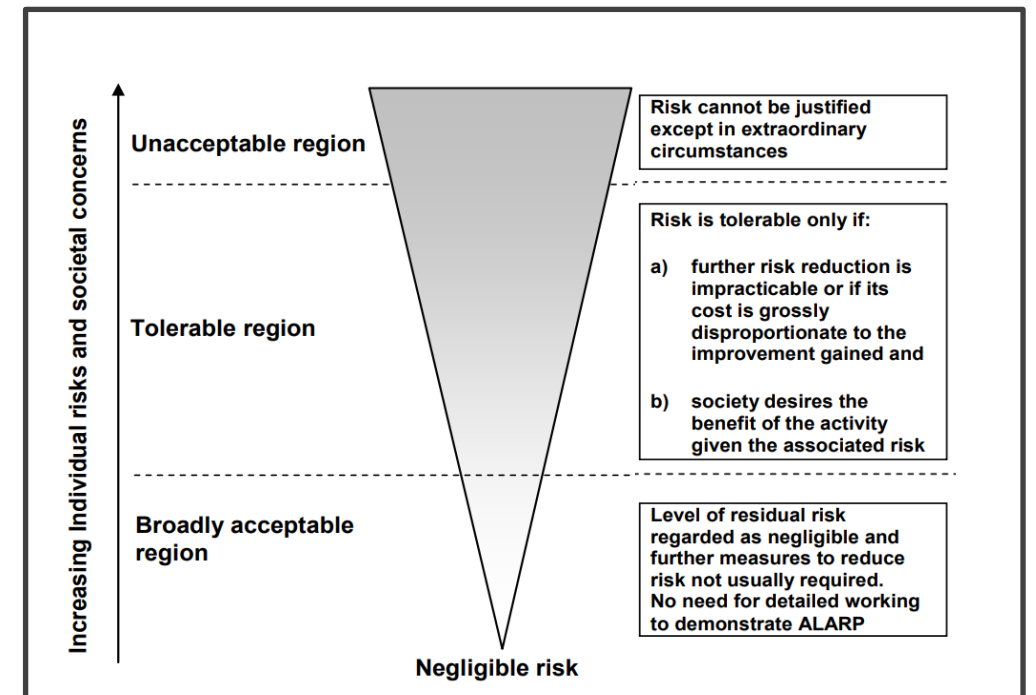
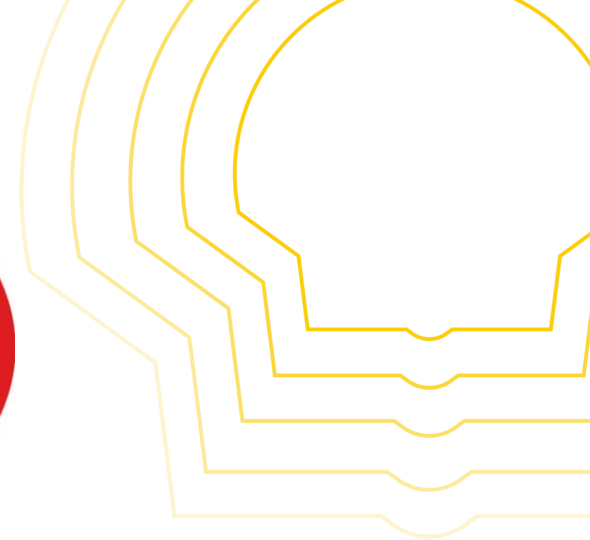
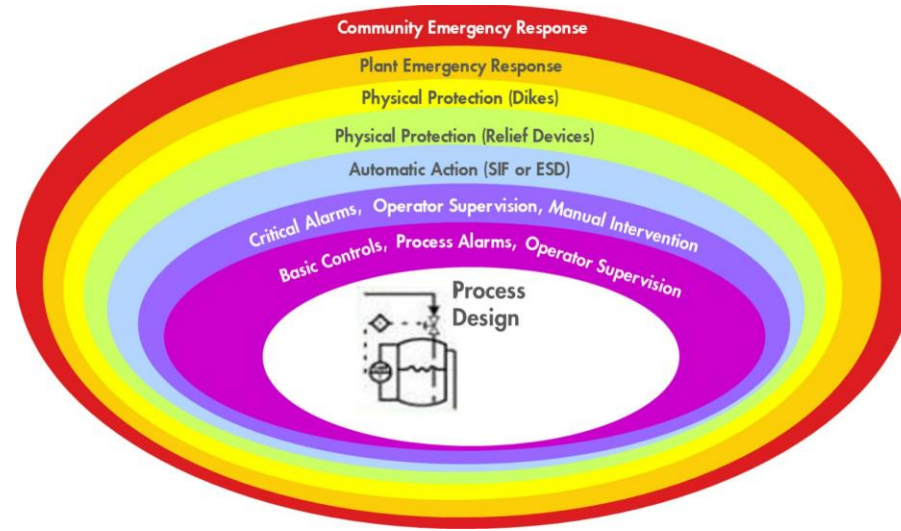
# Holland Hydrogen 1 Construction





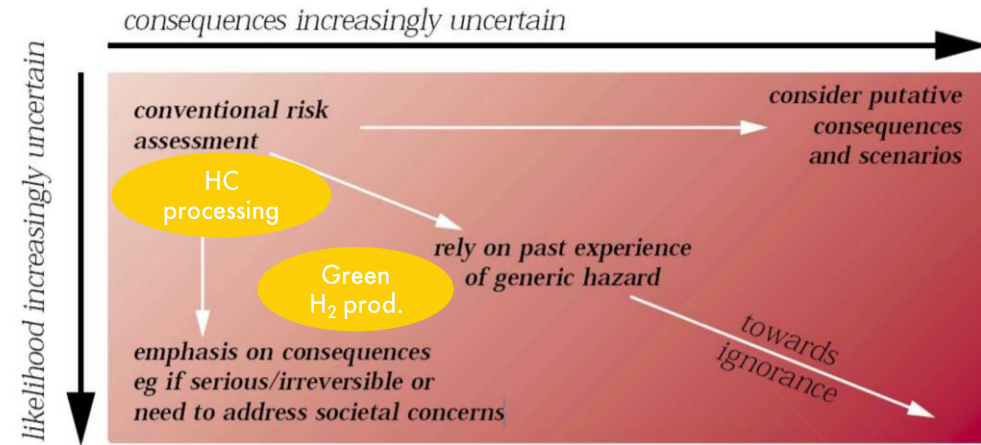
# Safe Design Philosophy

- Laws, regulations
- Codes & standards
- Vendor best practices
- Internal Shell standards
- Eliminate / substitute hazards
- Reduce risk to ALARP by adding valid barriers



# Risk Assessment Challenges for H<sub>2</sub> Production Plant Designs

- Gaps in laws, regulations codes and standards
- Uncertain event frequencies and consequences
- Standard tools for leak effect / QRA modelling not always sufficient
- Verification of effectiveness of novel barriers



- ➔ Project risk and potential inconsistency in safety standards across the industry
- ➔ Potential overdesign of safeguarding, avoidable cost
- ➔ Additional safety margin or comprehensive studies including model qualification
- ➔ No credit for risk reduction unless validated!

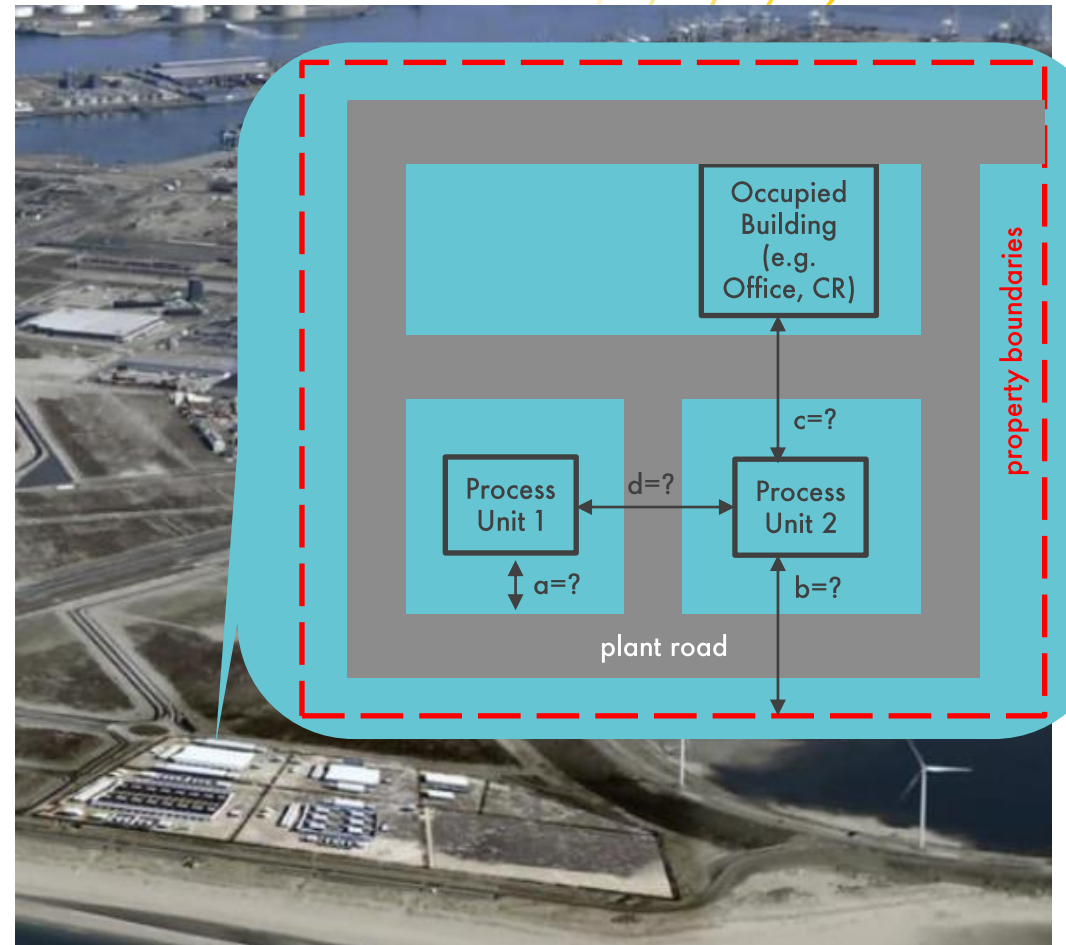
# Site Selection & Layout

## Drivers

- People Health / Safety (occupied building risk, access & escape, public risk, noise)
- Availability (asset damage risk, etc.)
- Cost effectiveness (piping length, insurance, barriers)
- Constructability & Maintainability

## Challenges

- Hardly dependable guidance by OEM, regulations, codes & standard
- Minimum Separation distances =  $f$  (operating pressure, congestion / confinement, mitigation)



- Time-consuming and costly iterative, multi-disciplinary optimization
- Potential cost escalation (in particular for small plots)

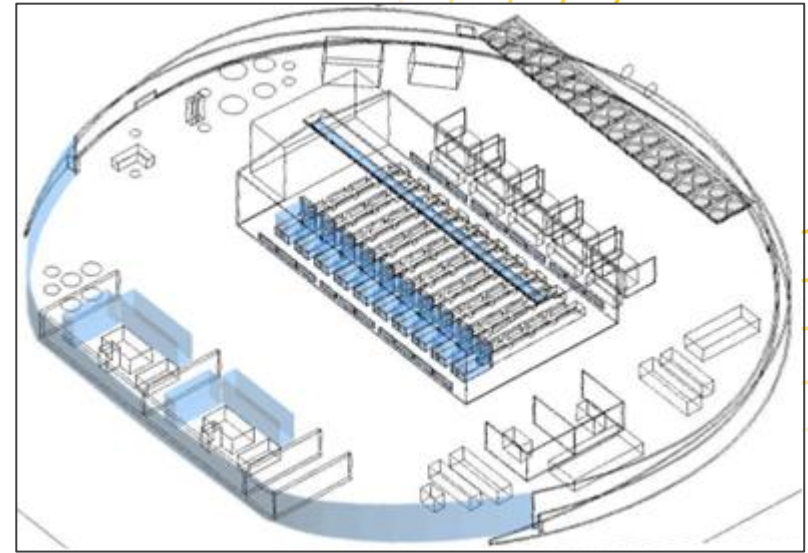
# Electrolyzer Building

## Objective & Requirements:

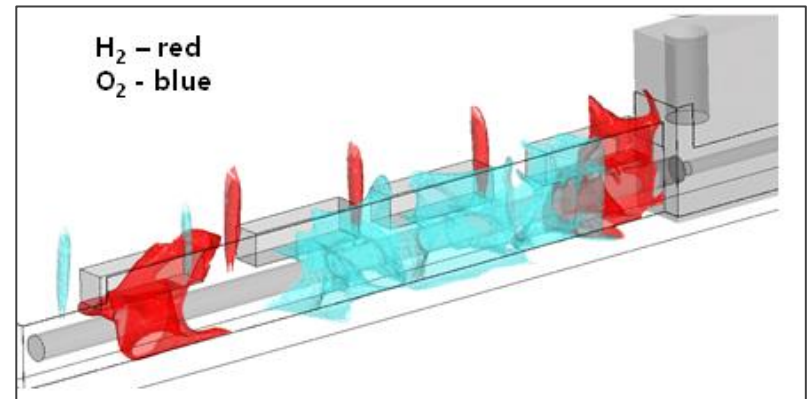
- Climate control as per OEM requirements
- Minimum ventilation as per ATEX standard for zone NE
- Fire & Explosion (F&G) safety and structural integrity

## Challenges

- Building excluded from vendor package
- Uncertainties in H<sub>2</sub> leak rates / frequencies
- Complex CFD studies for evaluation of ventilation and explosion risk



Geometry for HVAC design investigations



Calculated H<sub>2</sub> clouds (LEL) and oxygen clouds (23 %-vol)



# Conclusion: H<sub>2</sub> Industry needs concerted efforts

## Common awareness and standardization:

- Safe design methodologies
- Major hazardous scenarios and safeguarding requirements
- Electrolyzer plant specific separation distances

## Advancement in risk prediction:

- Global sharing on equipment failure and barrier performance
- H<sub>2</sub> ignition / explosion probability and consequence prediction

## Equipment design and testing:

- Development / validation of effective barriers and performance criteria
- Electrolyzer OEM support in design integration or fully modular designs





# Q&A

