



A MODEL FOR ASSESSING THE RISK OF LIQUID HYDROGEN TRANSPORT THROUGH ROAD TUNNELS

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INTRODUCTION

Hydrogen has the potential to help mitigate the current rapid climate change and achieve the goals of the <u>European Green Deal</u>:

- To reduce greenhouse gas emissions by at least 50% by 2030 compared to the '90;
- > To achieve climate neutrality in Europe by 2050.





In the short-term perspective **delivery of hydrogen by road transport as liquid** might represent the optimal solution, especially for long distances.

INTRODUCTION

- Liquid hydrogen (LH₂) presents different hazards and risks compared to those related to the more commonly known compressed gaseous hydrogen ^[1]
- After an accidental release of LH₂, in fact, <u>the flammable</u> <u>cloud might be significantly larger than that induced by a</u> <u>gaseous hydrogen release</u> due to the high density and vaporization ^[2]

• The consequences of a LH₂ leakage might be much more severe in a road tunnel, since the hydrogen mixture can be trapped by the tunnel ceiling increasing the risk of explosion ^[3]



Feared events associated with the trasport of liquid hydrogen. Source: PRESLHY Project Deliverable D6.3 Recommendations for RCS

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Experiments and/or simulations of LH₂ release <u>in the open</u>

Simulations of LH₂ release in road tunnels

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KNOWLEDGE GAP

Most of the studies have prevalently focused on the consequences of LH₂ releases in open spaces, but very few authors have dealt with their effects in confined spaces, such as tunnels.

SCOPE

> To develop a 3D CFD model of LH_2 release and dispersion in a road tunnel for assessing the potential negative effects on users (e.g., in the event of deflagration).

METHODOLOGY

The results of the CFD simulations (e.g., the amount of hydrogen contained within the flammable cloud) have been combined with established simplified consequence methods to estimate the overpressures generated from a potential hydrogen deflagration.

ROAD TUNNEL DESCRIPTION

GEOMETRIC AND FUNCTIONAL CHARACTERISTICS

- 1 km-long unidirectional road tunnel, straight, flat, with an emergency exit located in the middle of the tunnel length;
- Cross-section: 63 m² (2 lanes of 3.75 m, two sidewalks of 1 m, and two shoulders of 0.5 m);
- Only natural ventilation due to the piston effect of vehicles in motion ^[1].

	Tunnel walls (concrete)	Road pavement (asphalt mixture)
Thickness	0.5 m	0.4 m
Density	2585 kg/m ³	2275 kg/m ³
Thermal conductivily	1.67 W/m/K	0.56 W/m/K
Specific heat	0.94 kJ/kg/K	0.88 kJ/kg/K



MATERIAL PROPERTIES

[1] Directive 2004/54/EC, European Parliament and Council, Official Journal of the European Union, 2004.

ACCIDENT SCENARIOS

- Accidental release of LH₂ from a road tanker as a consequence of a traffic accident that generates a hole at the bottom rear side of the road tanker, the diameter of which was assumed to be 50 mm;
- Five different locations equally spaced along the tunnel have been simulated (i.e., 165, 335, 500, 670, and 835 m from the entrance portal of the tube).

Road tanker characteristics [1]



Tank volume = $45 m^3$ Tank capacity = 2500 kgTank working pressure = 4 barStorage temperature = 20 K Mass flow rate

 $\dot{m} = 7.7 \text{ kg/s}$

Duration of the release

 $t = 5.4 \min$

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ROAD TUNNEL DESCRIPTION

SCHEMATIZION OF QUEUED VEHICLES AND PEOPLE EVACUATION PROCESS

- Vehicles are schematized as parallelepipeds with dimension: 6 m (length) × 1.8 m (width) × 1.5 m (height);
- Safety distance between the vehicles upstream of the LH₂ road tanker: **2 m**;
- Traffic composition: 75% cars, 25% heavy vehicles (including 2% buses);
- Average occupancy rate: **2 people per vehicle**;
- Pre-movement time (detection + reaction time):
- People movement speed: **0.5 m/s**.



150 s

CFD SIMULATION CODE

Simulations have been carried out using ANSYS Fluent, version 2022 R1



Multiphase model \longrightarrow The transient two-phase flow was simulated by the <u>mixture model</u> [1]Liquid phase \longrightarrow Liquid hydrogen;
Gas phase \longrightarrow Hydrogen-air mixture;
All gases are assumed to be incompressible (Mach number ≤ 1.0).

The mass transfer from the liquid phase to the gas phase and vice versa is governed by the **evaporationcondensation Lee model** with saturation temperature set to 20.27 K.

Turbulence modelTurbulence closure solved by the $\underline{k-\varepsilon \ model}$ because found as the
most appropriate when dealing with gas dispersion in the presence of
obstacles ^[2], as well as to account for any buoyancy effect ^[3]

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[3] Xie, Y., Lv, N., Wang, X., Wu, D. and Wang, S., Thermal and fire characteristics of hydrogen jet flames in the tunnel at longitudinal ventilation strategies, Fuel, 306, 2021, 121659.

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[1] Witcofski, R.D. and Chirivella, J.E., Experimental and analytical analyses of the mechanisms governing the dispersion of flammable clouds formed by liquid hydrogen spills, *International Journal of Hydrogen Energy*, 9, No. 5, 1984, pp. 425–435.

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NUMERICAL MODELING

COMPUTATIONAL DOMAIN AND BOUNDARY CONDITIONS





[1] Ciambelli, P., Meo, M.G., Russo, P. and Vaccaro, S., Natural Vs Forced Ventilation During Fires In Relatively Short Road Tunnels, Proceedings of 29th Meeting of the Italian Section of the Combustion Institute, Pisa, Italy, 14-17 January 2006.

NUMERICAL MODELING





EVALUATION OF CONSEQUENCES OF A POTENTIAL DEFLAGRATION

• To predict the overpressure generated from a potential deflagration, <u>two simplified engineering</u> <u>correlations have been examined</u>, based on the mass of hydrogen contained within the cloud.



[1] Li, Y.Z., Fire and explosion hazards of alternative fuel vehicles in tunnels, Research Institutes of Sweden, Rapport 2018:20, 2018.

[2] Liu, J., Yan, Q. and Wu, J., Analysis of blast wave propagation inside tunnel, Transactions of Tianjin University, 14, No. 5, 2008, pp. 358–362.

[3] Silvestrini, M., Genova, B. and Trujillo, F.J.L., Energy concentration factor. A simple concept for the prediction of blast propagation in partially confined geometries, *Journal of Loss Prevention Process in the Process Industries*, 22, No. 4, 2009, pp. 449–454.

OVERPRESSURE ESTIMATED WITH THE SIMPLIFIED METHOD

• Overpressures over distance as a consequence of the hydrogen deflagration within the investigated tunnel tube for different ignition times when the leakage occurs in the middle of the tunnel length.



• The <u>Eisenberg probit function</u>^[1] was used to correlate the overpressure (P_s) with the probability of human falatity (P_r) due to lung hemorrhage $\longrightarrow Y = -77.1 + 6.91 \cdot \ln(P_s)$



[1] LaChance, J., Tchouvelev, A. and Engebo, A., Development of uniform harm criteria for use in quantitative risk analysis of the hydrogen infrastructure, *International Journal of Hydrogen Energy*, 36, No. 3, 2011, pp. 2381–2388.

 By knowing the position of each user within the tunnel tube during the evacuation process it was possible to estimate the number of people exposed to a given overpressure and their probability of fatality.



- A 3D CFD model of liquid hydrogen release from a tanker within a road tunnel was developed and validated against experimental tests and numerical simulations;
- The results showed that the worst-case scenario is when the release occurs in the middle of the tunnel length, and the potential ignition of the flammable hydrogen cloud after 90 s from the release.
- The <u>number of potential fatalities</u> due to lung hemorrage as a consequence of the deflagration significantly increases with the pre-movement time of the escaping users. This means that the evacuation process should start as soon as possible when an accidental release of LH_2 occurs in a road tunnel.

CONCLUSIONS

FURTHER STUDIES

> Development of a **CFD model to estimate the overpressures** due to hydrogen deflagration





THANK YOU

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