



# EXPERIMENTAL CHARACTERIZATION OF THE OPERATIONAL BEHAVIOR OF A CATALYTIC RECOMBINER FOR HYDROGEN MITIGATION

Krenz, S.R., Reinecke, E.-A., Tanaka, H., Bentaib, A., and Chaumeix, N.

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### Introduction



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# Introduction: Hydrogen Risk

- Flammability Range: 4 to 75 vol%
- Density: 0.084 kg/m<sup>3</sup>
- Risk
  - Limited in outdoor/open spaces
  - Greater in enclosed spaces
- Risk Mitigation
  - Forced/Natural ventilation
  - Ventilation + Recombiners
  - Recombiners



R Kelm et al., Simulation of H2 mixing and PAR operation during accidental release in an LH2 carrier engine room, ICHS, 2021



Relm et al., Simulation of H2 mixing and PAR operation during accidental release in an LH2 carrier engine room, ICH5, 2021



# Passive Auto-Catalytic Recombiners

• Chemically convert hydrogen into water

$$H_{2(g)} + \frac{1}{2}O_{2(g)} \xrightarrow{Pt \setminus Pd} H_2O_{(g)} + 240 \frac{kJ}{mole}$$

• Reduce hydrogen accumulation







#### Enersys-Hawker Hydrogen Eliminator





# Passive Auto-Catalytic Recombiners



Objective: Study the operational behavior of the Hawker Eliminator

PAR from Nuclear Power Plant



Enersys-Hawker Hydrogen Eliminator





# Agenda

#### Introduction

Passive Auto-Catalytic Recombiners

- Experimental Setup
- Test Procedure
- Results

#### Conclusion

Acknowledgements



# Experimental Setup: Instrumentation

**Measurement Devices** 

- Pressure sensor
- Thermal conductivity sensor
- Oxygen sensor
- Humidity sensor
- Thermocouple







# Experimental Setup: Instrumentation

TR-4-17 and KR-4-16











## **Experimental Setup: Instrumentation**





### Test Procedure



• TR-4-17 and KR-4-16 TR-4-16 • TR-4-10 TR-4-13 • TR-4-14 TR-4-12 and KR-4-20

A: Start of Hydrogen Injection

**B: Start of Reaction** 

C: Catalyst Light-off

D: Start of quasi–Steady State phase

E: End of quasi-Steady State, Injection Stopped, and Start of Dynamic phase

F: End of Dynamic and Start of Purging



### Test Procedure

 $H_2 \leftarrow$ 

h	Test #	Injection	Injection	Injection	Injection
$\frac{dn}{dn} = \dot{n} \cdot \cdot$		Rate 1	Rate 2	Rate 3	Rate 4
$\frac{dt}{dt} = n_{in} - q_{j}$		(n-m³/h)	(n-m³/h)	(n-m³/h)	(n-m³/h)
	1	0.10	0.15	0.20	0.25
Steady State $\frac{dn}{dt} = 0$	2	0.10	0.15	-	-
	3	0.25	0.20	0.15	0.10
	4	0.20	-	-	-
v	5	0.25	0.20	0.15	0.10
$\dot{r}=\dot{n}_{in}$	6	0.15	-	_	-



### Results: Start-up

 $H_{2(g)} + \frac{1}{2}O_{2(g)} \rightarrow H_2O_{(g)} + 240 \frac{kJ}{mole}$ 

Hydrogen concentration and average catalyst temperature at the initial reaction start.

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Test #	Hydrogen	Average Catalyst	Time
	Concentration	Temperature	(min)
	(vol.%)	(°C)	
1	0.25	19.0	8.1
2	0.16	20.7	5.6
3	0.23	21.3	3.1
4	0.54	16.2	8.1
5	0.51	18.1	6
6	0.42	20.1	7.8

#### Average catalyst light off temperature and hydrogen concentration

Test #	Average	Hydrogen	Time
	Catalyst	Concentration	(min)
	Temperature	(vol.%)	
	(°C)		
1	22.7	0.53	17.4
2	33.6	0.45	22.7
3	34.5	0.81	11.2
4	17.4	0.71	10.8
5	20.9	0.82	10.1
6	21.4	0.59	11.4



### Results: Steady-states





TR-4-10

TR-4-14

• TR-4-17 and KR-4-16

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TR-4-16 🛆

TR-4-13 🗆

# Results: Temperature Profile



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### **Results: Recombination Rates**





### Conclusion

Characterized:

• Recombination rates

Key Characteristics:

- Fast start up
- Prolonged use

#### Observation:

- Opposite temperature profile than convectional recombiners
  - Possible Explanations:
    - Lower flow velocities
    - Not as well-developed boundary layers

Future work:

- Numerical model
- Lower temperatures
- Higher Injection Rates









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# Thank you!













#### **Questions**? in $\langle \rangle$ sh.krenz@fz-juelich.de Shannon Krenz www.stacy-project.eu/en KWANSEI GAKUIN JÜLICH CNIS Forschungszentrum INSTITUT DE RADIOPROTECTION ET DE SÛRETÉ NUCLÉAIRE



# Results (continued)

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# Results (continued)





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# Results (continued)





# Results (continued)





# Passive Auto-Catalytic Recombiners

