

An improved passive scalar model for hazardous H₂-Air ignition prediction

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1. Introduction
2. Previous model framework
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Motivations

- Increasing use of hydrogen (industry, transport, ...)
- Extended flammability limits
- Low minimum ignition energy
- High-pressure storage (up to 700 bars)

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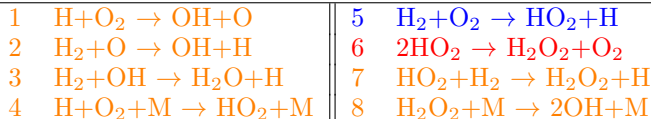
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- Extended flammability limits
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Objectives

- Accurate and low-cost model to predict H₂ ignition
- Extend validity for higher pressure

For H₂-Air, detailed mechanisms use around 20 reactions¹.

Ignition alone can be described with only 8 reactions²:



¹F.A. Williams et al. *Chemical-kinetic mechanisms for combustion applications*, University of California, San Diego. version 2016-12-14, last accessed on 2023-02-22.
URL: <http://web.eng.ucsd.edu/mae/groups/combustion/mechanism.html>.

²P. Boivin. “Reduced-kinetic mechanisms for hydrogen and syngas combustion including autoignition”. PhD. Universidad Carlos III de Madrid, Dec. 2011.

Ignition can be solved as a linear system³:

$$\frac{d\bar{C}}{dt} = \mathbf{A}\bar{C} + \bar{\epsilon}$$

with the radicals vector $\bar{C} = [C_{\text{H}}, C_{\text{O}}, C_{\text{OH}}, C_{\text{HO}_2}, C_{\text{H}_2\text{O}_2}]^T$,

$$\text{the Jacobian } \mathbf{A} = \begin{bmatrix} -l_1 - l_4 & l_2 & l_3 & l_7 & 0 \\ l_1 & -l_2 & 0 & 0 & 0 \\ l_1 & l_2 & -l_3 & 0 & 2l_8 \\ l_4 & 0 & 0 & -l_7 & 0 \\ 0 & 0 & 0 & l_7 & -l_8 \end{bmatrix} \text{ and } \bar{\epsilon} = \begin{bmatrix} \omega_5 \\ 0 \\ 0 \\ \omega_5 \\ 0 \end{bmatrix}$$

$$l_1 = k_1 C_{\text{O}_2}, l_2 = k_2 C_{\text{H}_2}, l_3 = k_3 C_{\text{H}_2}, \dots$$

³P. Boivin, A.L. Sánchez, and F.A. Williams. “Analytical prediction of syngas induction times”. In: *Combust. Flame* 176 (2017), pp. 489–499.

Using the largest eigenvalue λ that rapidly dominates, the system can be reduced to a scalar equation⁴:

$$\frac{dC_\eta}{dt} = \lambda C_\eta + \epsilon_\eta$$

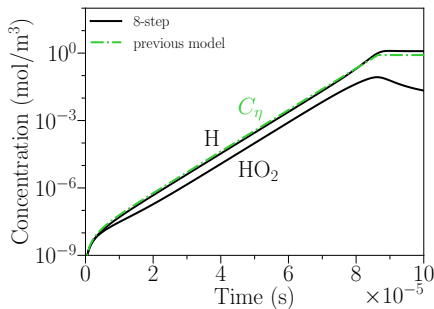


Figure: Concentrations evolution during isobaric homogeneous ignition process ($\varphi=1.0$, $p=1$ atm, $T_0=1100$ K)

⁴S. Taileb et al. “Lattice-Boltzmann modeling of lifted hydrogen jet flames: A new model for hazardous ignition prediction”. In: *Combust. Flame* 245 (2022), p. 112317.

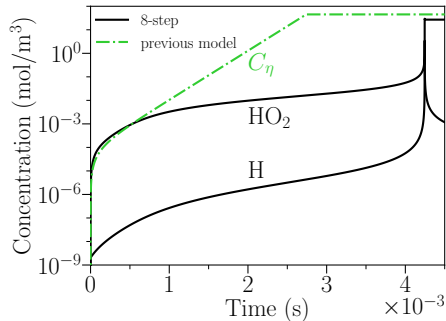


Figure: Concentrations evolution during a homogeneous isobaric ignition process ($\varphi=1.0$, $p=50$ atm, $T_0=1000$ K)

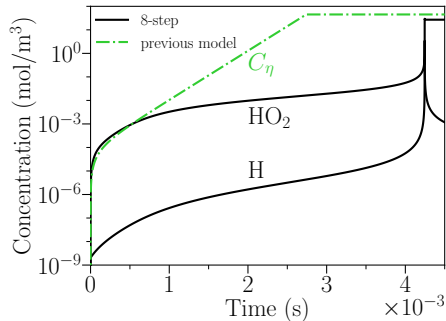


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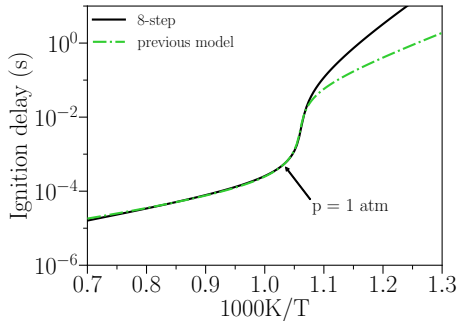


Figure: Autoignition delay as a function of temperature during a homogeneous isobaric process ($\varphi=1.0$)

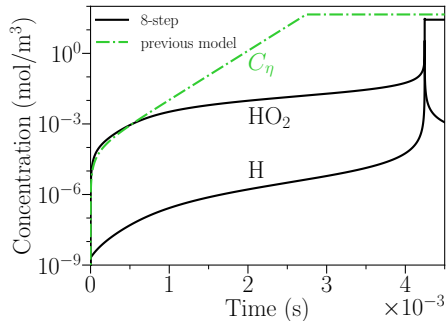


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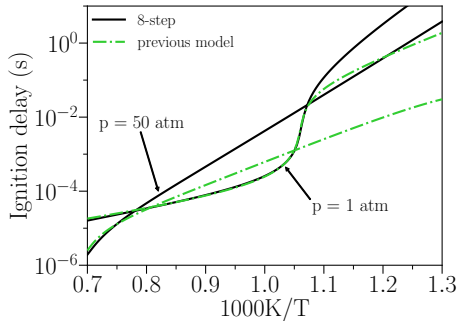


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Linearisation of the reaction 6 term⁵
 $(\text{HO}_2 + \text{HO}_2 \rightarrow \text{H}_2\text{O}_2 + \text{O}_2)$ into the
 new Jacobian:

$$\begin{bmatrix} -l_1 - l_4 & l_2 & l_3 & l_7 & 0 \\ l_1 & -l_2 & 0 & 0 & 0 \\ l_1 & l_2 & -l_3 & 0 & 2l_8 \\ l_4 & 0 & 0 & -l_7 - 4l_6 & 0 \\ 0 & 0 & 0 & l_7 + 2l_6 & -l_8 \end{bmatrix}$$

$$l_6 = k_6 C_{\text{HO}_2}^* (C_\eta)$$

$$\frac{dC_\eta}{dt} = \lambda(C_{\text{HO}_2}^*) C_\eta + \epsilon_\eta$$

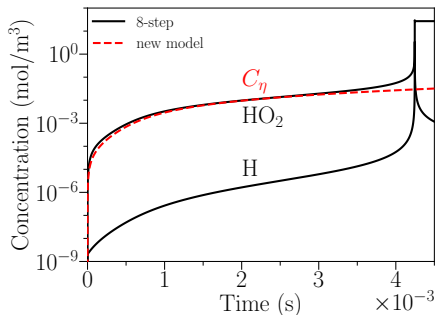


Figure: Concentrations evolution during a homogeneous isobaric ignition process ($\varphi=1.0$, $p=50$ atm, $T_0=1000$ K)

⁵Wenkai Liang and Chung K Law. “An analysis of the explosion limits of hydrogen/oxygen mixtures with nonlinear chain reactions”. In: *Phys. Chem. Chem. Phys.* 20 (2018), pp. 742–751.

High activation energy development of λ :

$$\lambda(\theta) = \lambda e^{\theta} \text{ with } \theta = \beta \frac{T - T_0}{T_0}$$

The thermal runaway problem leads to: $\theta(C_\eta) = \ln \left(1 + \frac{q C_\eta^2}{2\lambda} \right)$.

The final scalar reaction rate now includes a correction term:

$$\frac{dC_\eta}{dt} = \lambda(C_{\text{HO}_2}^*) C_\eta + \frac{q}{2} C_{\text{HO}_2}^{*3} + \epsilon_\eta = \dot{\omega}_\eta$$

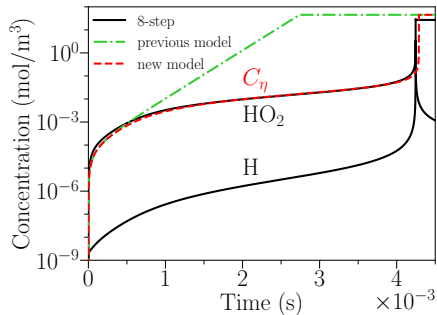


Figure: Concentrations evolution during isobaric homogeneous ignition process ($\varphi=1.0$, $p=50$ atm, $T_0=1000$ K)

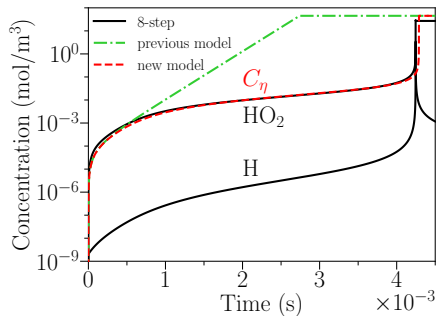


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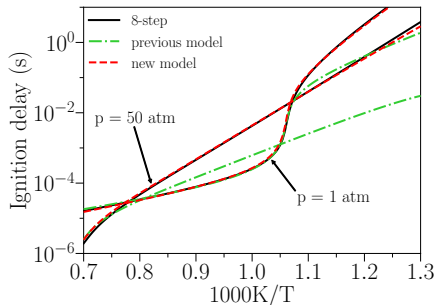


Figure: Autoignition delay as a function of temperature during a homogeneous isobaric process ($\varphi=1.0$)

Classic conservation equations of thermal flow:

- Only considering the main species (H_2 , O_2 , diluent)
- No reaction nor heat release
- Adding the self-reacting scalar C_η , not used to solve the flow and following a classic advection-diffusion-reaction equation:

$$\frac{\partial C_\eta}{\partial t} + u_\alpha \frac{\partial C_\eta}{\partial x_\alpha} = \frac{\partial}{\partial x_\alpha} \left(D_\eta \frac{\partial C_\eta}{\partial x_\alpha} \right) + \dot{\omega}_\eta$$

The previous model used $D_\eta = D_H$

The improved model uses the eigenvector \bar{V} of λ :

$$D_\eta = \frac{\sum_k D_k V_k}{\sum_k V_k}$$

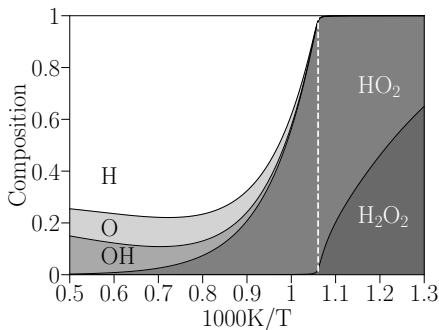


Figure: Composition of the radical pool given by the eigenvector \bar{V} ($\varphi = 1.0$, $p = 1$ atm)

2D double mixing layer:

- Hot air (1200 K)
- Cold diluted H₂ (50% in volume)
- High pressure (50 atm)
- Weak turbulence ($\tau_t > \tau_i$)
- 4.5mm × 4.5mm (500 × 500 points)

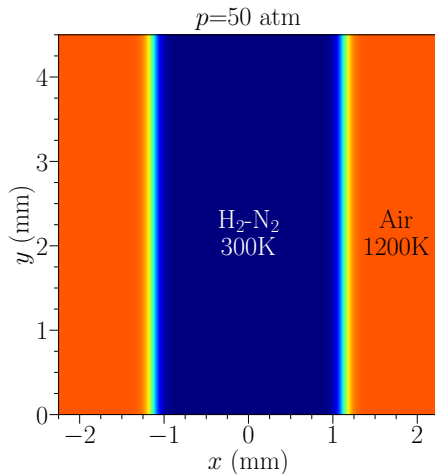


Figure: Initialization of the mixing layer

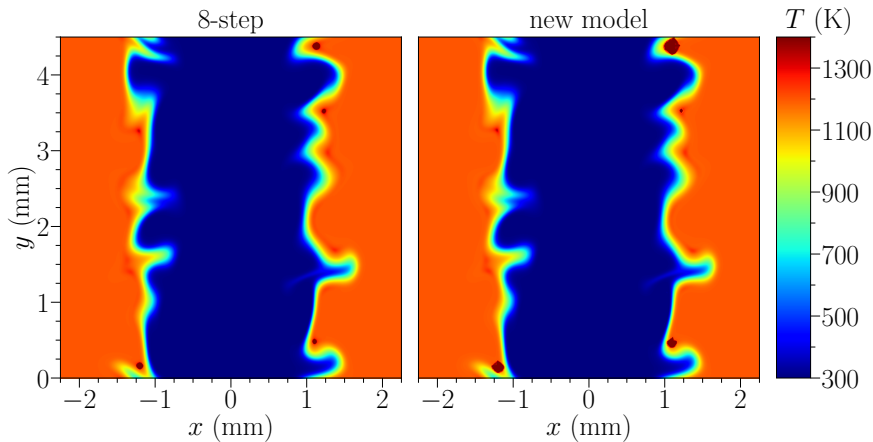
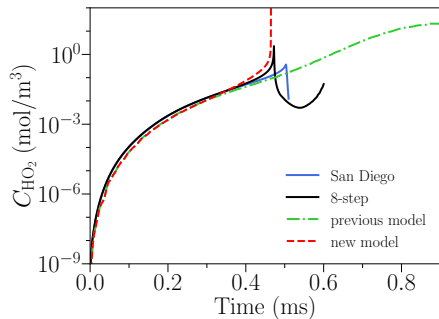


Figure: Temperature field (reconstructed for the scalar model) after ignition



case	τ_i (ms)	cost
San Diego	0.497	43.7
8-step	0.472	9.1
Previous model	0.826	1.0
New model	0.464	1.0

Figure: Evolution of C_{HO_2} and C_η at the first kernel to ignite.

Conclusion:

- Considering the nonlinear reaction $\text{HO}_2 + \text{HO}_2 \rightarrow \text{H}_2\text{O}_2 + \text{O}_2$
- Adding a correction term for thermal runaway
- Evaluating the scalar diffusion with the eigenvector
- Accurate for extended temperature and pressure ranges at a low-cost

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Perspectives:

- Assessment of self-ignition risks for high-pressure tank leakage.
- Investigation of the potential of the model for the study of igniters.

Thank you

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