

PRE-SLHY

WP3 – Release and mixing: UU update

D. Cirrone, D. Makarov, V. Molkov

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Pre-normative REsearch for Safe use of Liquid HYdrogen

223
1966



UU - WP3 activities plan



- ✓ Analysis of the similarity law for momentum dominated cryogenic jets for use in calculation of hazard distances: validation against SNL tests
- Analysis of the applicability of notional nozzle theory and volumetric release source concept for prediction of concentration decay in cryogenic under-expanded jets:
 - ✓ Low pressure releases ($P < 10$ bar): validation against SNL tests
 - High pressure releases ($P > 10$ bar): validation against ICESAFE and PRESLHY experiments performed by KIT (E3.1)
- Perform simulations of experiments on multi-phase releases:
 - Contemporary engineering tool for evaluation of mass flow rate from LH2 tank with inclusion of conjugate heat transfer: HSE experiments (E3.5)
- Studies on formation of cryogenic mixtures of H₂/O₂ and H₂/air (connected to WP4-Ignition)

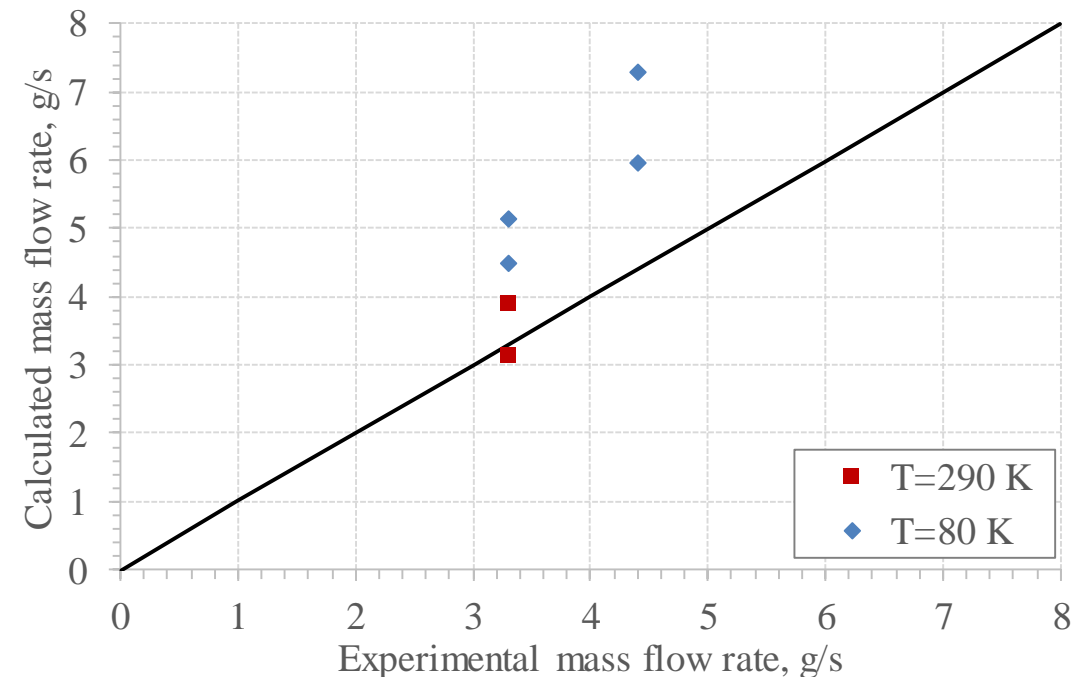
Release source modelling

Jet fire tests performed at KIT - ICEFUEL

The under-expanded jet theory developed at Ulster was employed to model cryogenic and warm hydrogen releases by KIT at ICEFUEL facility

(Breitung et al., 2009).

Release conditions	
Temperature, K	80, 290
Pressure, bar	3 – 20
Diameter, mm	2, 4

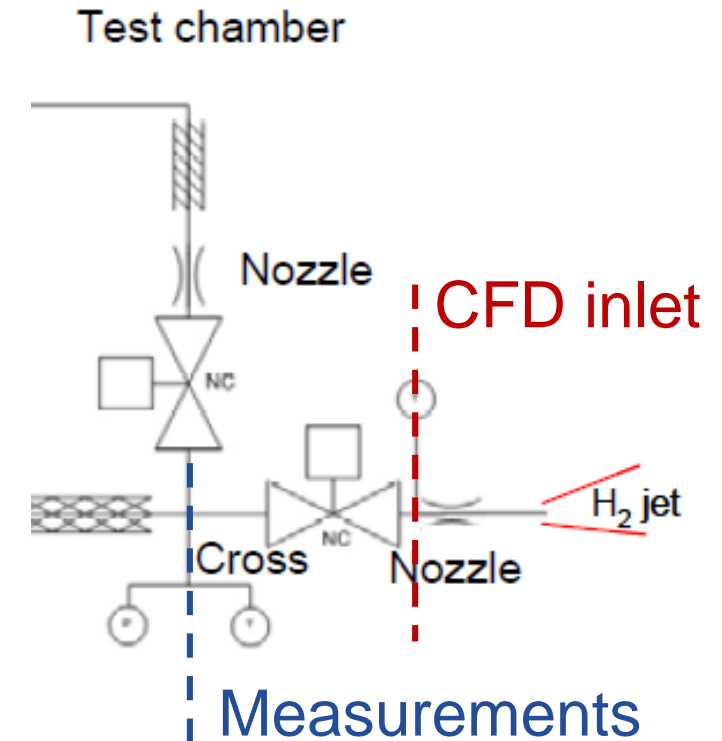
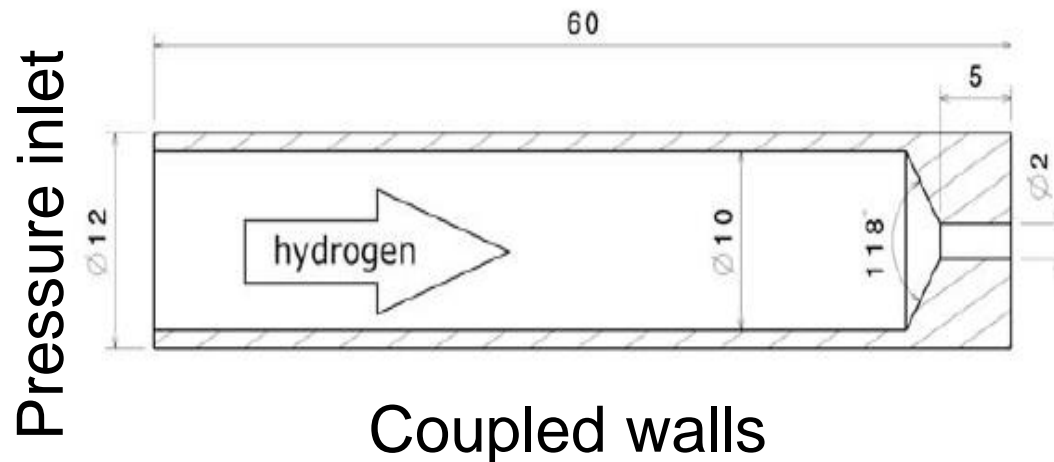


CFD simulations to investigate reasons for mass flow rate deviation:

- Losses and heat transfer in the release pipe
- Effect of cryogenic release temperature
- Calculate notional nozzle conditions for jet fires simulations (WP5)

Release source: CFD modelling

Problem formulation



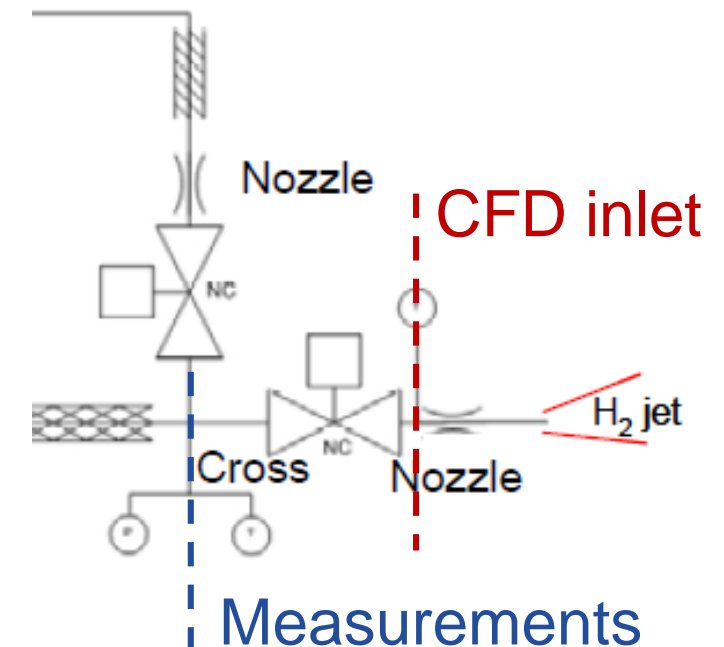
- Density based compressible explicit solver
- LES dynamic Smagorinsky-Lilly model
- Cylindrical domain with dimensions 7 cm (radius) x 18 cm (length)
- Hexahedral mesh with ~500 thousands CVs
- Inclusion of conjugate heat transfer in simulations

Effect of inlet temperature on \dot{m}

Simulation results

Test with $T=80\text{ K}$ $P=14\text{ bar}$ measured at the cross.

Case	Mass flow rate, g/s
CFD – $T_{in}=80\text{K}$	4.3
CFD – $T_{in}=100\text{K}$	3.8
CFD – $T_{in}=120\text{K}$	3.5
CFD – $T_{in}=150\text{K}$	3.2
Experiment	3.3



- Heat transfer causes a 9% difference on the calculated mass flow rate
- Important: location of temperature sensor!

Thank you for your attention!

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